### AFOEHL REPORT 89-068EQ0686GEF



# Compliance Testing of Eielson AFB Central Heating and Power Plant, Coal-Fired Boiler No. 4, Eielson AFB AK

JAMES A. GARRISON, Maj, USAF, BSC

**JULY 1989** 



**Final Report** 

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AF Occupational and Environmental Health Laboratory (AFSC)
Human Systems Division
Brooks Air Force Base, Texas 78235-5501

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The Public Affairs Office has reviewed this report, and it is releasable to the National Technical Information Service, where it will be available to the general public, including foreign nations.

This report has been reviewed and is approved for publication.

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Chief, Air Quality Function

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REPORT DOCUMENTATION PAGE				Form Approved OMB No 0:04-0188	
10 REPORT SECURITY CLASSIFICATION UNCLASSIFIED	REPORT SECURITY CLASSIFICATION 16 RESTRICTIVE MARKINGS N/A				
20 SECURITY CLASSIFICATION AUTHORITY		3 DISTRIBUTION/AVAILABILITY OF REPORT Approved for public release.			
26 DECLASSIFICATION/DOWNGRADING SCHEDUN/A	ULE	Distribution is unlimited.			
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At the request of HQ 343 CSG/DEEV and HQ AAC/SGPB, source compliance testing (particulate and visible emissions) of Boiler No. 4 in the Eielson AFB Central Heating and Power Plant was conducted on 7-15 June 1989. Testing was performed to determine compliance with regards to the renewal of Alaska Department of Environmental Conservation Air Quality Control Permit to Operate #8331-AA001. Boiler No. 4 was tested on 12 and 14 Jun 89. On 12 June results indicated that visible emissions standards were met; however, particulate emissions standards were not met. The boiler was retested on 14 June and all emissions standards were met. All emission requirements for permit renewal have now been met.					
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22a NAME OF RESPONSIBLE INDIVIDUAL22b TELEPHONE (Include Area Code)22c OFFICE SYMBOLJames A. Garrison. Maj, USAF, BSC(512) 536-3305 AV 240 AF0EHL/ECQ				CE SYMBOL OEHL/ECQ	

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#### I. INTRODUCTION

On 7-15 June 1989, compliance emission testing for particulate and visible emissions was conducted on coal-fired boiler 4 at the Eielson AFB Central Heat and Power Plant (CH&PP), by personnel of the Air Quality Function, Consultant Services Division, Air Force Occupational and Environmental Health Laboratory (AFOEHL). This survey was requested by HQ 343 CSG/DEEV and HQ AAC/SGPB to determine visible and particulate emission compliance status with regards to the renewal of Alaska Department of Environmental Conservation (ADEC) Air Quality Control Permit to Operate #8331-AA001. Personnel involved with on-site testing are listed in Appendix A.

#### II. DISCUSSION

#### A. Background

On 7 January 88 Eielson AFB requested that ADEC renew Air Quality Control Permit to Operate #8331-AA001 (Appendix B) for the CH&PP (Figures 1 and 2). As a condition of the permit renewal process and prior to issue of the new Air Quality Control Permit to Operate #8831-AA001, ADEC required source testing of a representative boiler in accordance with Title 40 Code of Federal Regulation Part 60 (40 CFR 60) Appendix A, Methods 1 through 5 (determination of particulate emissions) and 9 (visual determination of the opacity of emissions) to determine the maximum steam load at which the boilers will meet the applicable emission standards. Permit #8831-AA001 limits the operation of the boilers to the maximum steam load at which the associated visible and particulate emissions meet the applicable standards.

To demonstrate and maintain compliance with Alaska Administrative Code, Title 18, Environmental Conservation, Chapter 50 - Air Quality Control (18 AAC 50) and other rules set forth by ADEC, Eielson AFB requested that AFOEHL conduct stationary source emissions testing on a representative boiler to: (1) determine particulate emissions as specified in 40 CFR 60, Appendix A, Reference Methods 1-5, and (2) determine the opacity of visible emissions from the same boiler during Method 5 testing as specified in 40 CFR 60, Appendix A, Reference Method 9.

Source testing was accomplished during July 1988 on boiler 3. The boiler was tested twice at each of two operating capacities; 100,000 and 90,000 pounds of steam per hour. Boiler 3 failed to meet particulate standards; however, it did meet visible emissions standards. Boilers at the power plant were subsequently down-rated to 80% operating capacity by ADEC until further testing indicated standards could be met at a higher operating capacity.



Figure 1. Eielson AFB Central Heat and Power Plant



Figure 2. Eielson AFB Central Heat and Power Plant

#### B. Site Description

The CH&PP operates a total of six boilers for electrical power and steam production:

Boiler No./ Manufacturer	Steam Capacity (lb/hr)	Year Installed	Fuel
1/Springfield Boiler Co.	120,000	1950	coal
2/Springfield Boiler Co.	120,000	1950	coal
3/Springfield Boiler Co.	120,000	1950	coal
4/Springfield Boiler Co.	120,000	1950	coal
5/Garrette and Schafer	120,000	1954	coal
6/Garrette and Schafer	120,000	1954	coal

The CH&PP also operates five steam turbine generators for electrical power production. The turbines range in size from 2,500 to 10,000 kilowatts. A typical turbine is shown in Figure 3.

All boilers are spreader-stoker fired units with mechanical fly-ash collection systems. Each unit is fitted with a steam-operated soot blower to remove fly-ash and soot from heat exchanger tubing.

Air pollution control consists of individual multiclone dust collectors (see Figure 4) on each boiler. The multiclone dust collectors were manufactured by Western Precipitation Division - Joy Manufacturing Co. and consist of a number of cyclonic collectors operating in parallel. Each unit is located in the boiler exhaust duct upstream of the induced-draft fan.

The exhaust effluent from each boiler is ducted to a separate exhaust stack located on the roof of the CH&PP. Figure 5 shows the exhaust stack for boiler 4 during testing. All boiler exhaust stacks are similar to the one pictured in Figure 5.

#### C. Applicable Standards

The opacity, particulate and source testing regulations are defined under 18 AAC 50.050(a), 50.050(b) and 50.500, respectively (Appendix C). Paragraph 50.050(a) states that visible emissions, excluding condensed water

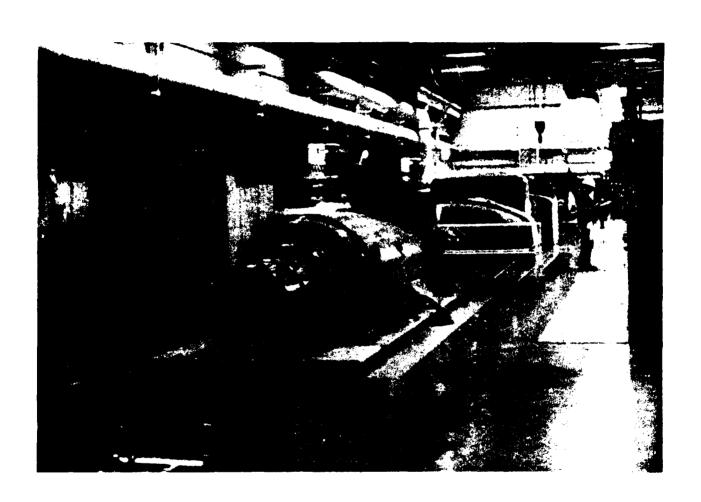


Figure 3. Steam Turbine Generator

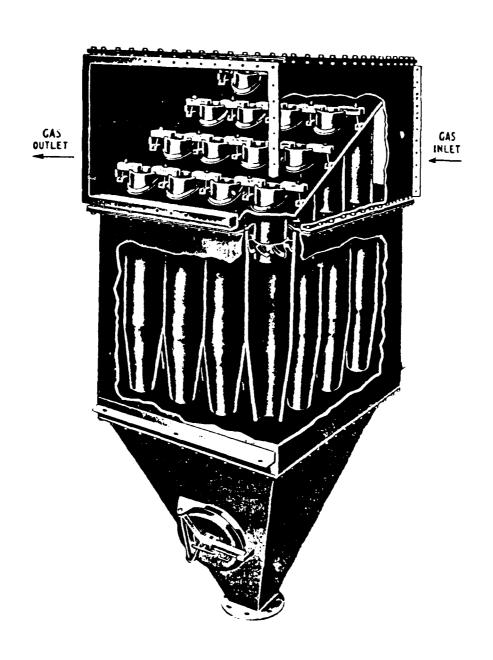
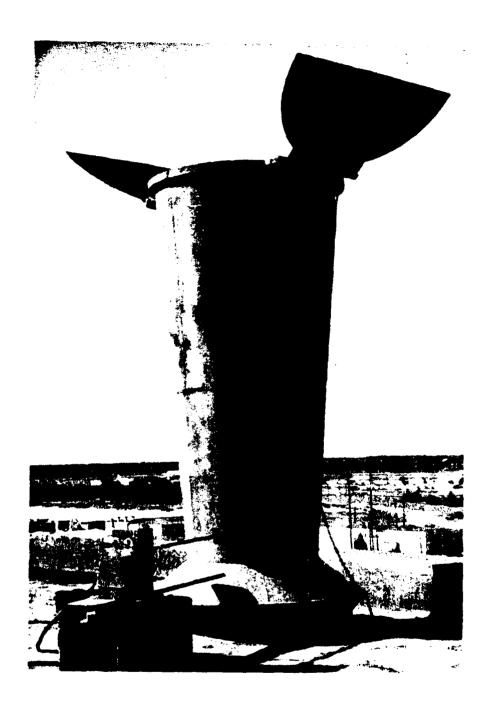


Figure 4. Multiclone Dust Collector



Tigure 5. Boiler 4 Exhaust Stack During Testing

vapor from an industrial process or fuel burning equipment, may not reduce visibility through the exhaust effluent by greater than 20% for a total of more than three minutes in any one hour.

Under 18 AAC 50.050(b), particulate matter emitted from industrial processes or fuel burning equipment may not exceed, per cubic foot of exhaust gas corrected to standard conditions, 0.1 grains per dry standard cubic foot (gr/dscf) for steam generating plants burning as fuel: (1) coal, and in operation before July 1, 1972 or (2) coal, and rated less than 250 million Btu per hour heat input.

Permit to Operate No. 8831-AA001, Exhibit B, reiterates the visible and particulate emissions standards imposed by 18 ACC 50.050(a) and (b).

#### D. Sampling Methods and Procedures

The permit to operate for the CH&PP limits the operation of the boilers to the maximum steam load at which the associated visible and particulate emissions meet standards. We analyzed particulate emissions data on site to determine the operating capacity which would meet emissions standards.

18 AAC 500 and Permit No. 8831-AA001 require that all emissions tests be conducted in accordance with the procedures and analysis methods specified in 40 CFR 60, Appendix A, Methods 1-5 and 9. Therefore, test methods, equipment, sample train preparation, sampling and recovery, calibration requirements, and quality assurance were done in accordance with the methods and procedures outlined in 40 CFR 60, Appendix A.

The boiler exhaust stacks are tapered and diverge from a 52 inch (in) outside diameter (OD) at the roof line to a 72 in OD at the top. The stack height is 14.2 feet (ft). The included divergent angle of the stack is approximately 7 degrees. Based on the relative small divergent angle, we considered the stacks to be straight ducts. Sampling ports were already in place and located 36 inches above the roof. Prior to the stack, exhaust gases pass through the induced draft fan, rectangular ducting and a transition to the stack located just below the roof. Figure 6 provides a schematic of the exhaust stack and associated duct work. Even though the sampling port location did not meet Method 1 criteria, the test team made the decision to use the existing sample ports since a similar configuration had been previously approved by ADEC personnel during source testing conducted in July 1988. Based on the port location, stack diameter at the sample port location and type of sample (particulate), a maximum number of 24 traverse points were used for emission evaluation.

Particulate samples were collected using the sampling train shown in Figure 7. The train consisted of a button-hook probe nozzle, heated stainless steel probe, heated glass filter, impingers and pumping and metering device. The nozzle was sized prior to each sample run so that the gas stream could be sampled isokinetically; in other words, the velocity at the nozzle tip was the same as the stack gas velocity at each point sampled. Flue gas velocity pressure was measured at the nozzle tip using a Type-S pitot tube connected to

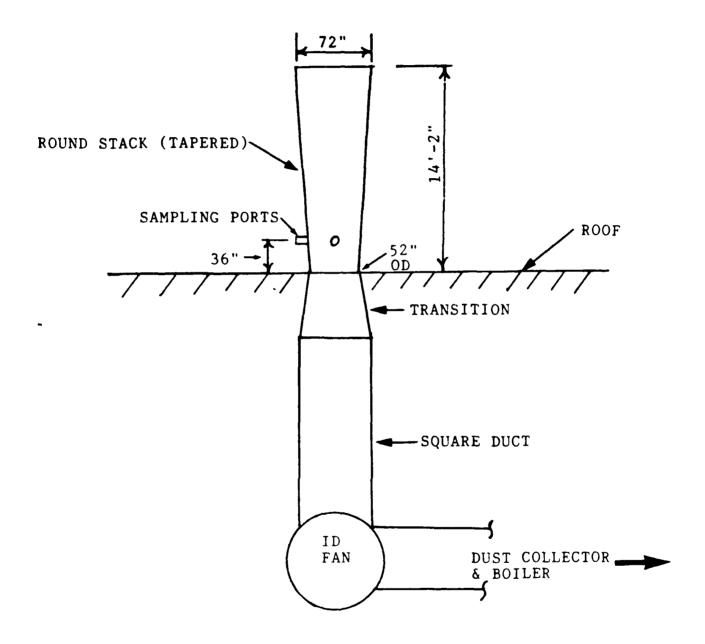


Figure 6. Exhaust Duct Transition

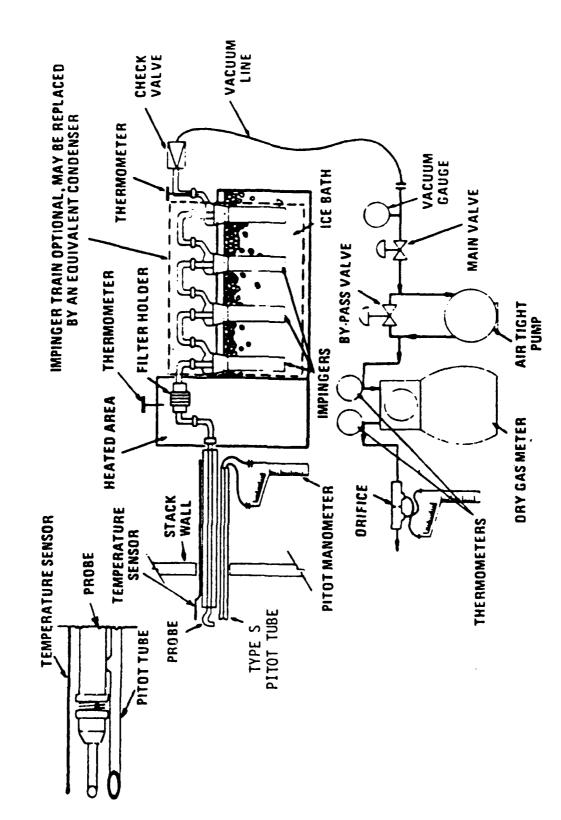


Figure 7. Particulate Sampling Train

a ten-inch inclined-vertical manometer. Type K thermocouples were used to measure flue gas as well as sampling train temperatures. The probe was heated to minimize moisture condensation. The heated filter was used to collect particulate materials. The impinger train (first, third and fourth impingers: modified Greenburg-Smith type, second impinger: standard Greenburg-Smith design) was used as a condenser to collect stack gas moisture. The pumping and metering system was used to control and monitor the sample gas flow rate. Calibration data are presented in Appendix D.

The time for each sampling run was 60 minutes (three sample runs make up a complete test); therefore, the sampling time per traverse point was 2.5 minutes. These sample times were applicable for all runs.

Prior to each test, a preliminary velocity pressure traverse was accomplished and cyclonic flow was determined. For acceptable flow conditions to exist in a stack, the average of the absolute value of the flow angle taken at each traverse point must be less than or equal to 20 degrees. The flow angle for the boiler 4 stack averaged 8 degrees.

During each sample run, a flue gas grab sample for ORSAT analysis (measures oxygen, and carbon dioxide for stack gas molecular weight determination and emissions correction) was taken. ORSAT sampling and analysis equipment are shown in Figures 8 and 9. Flue gas moisture content, also needed for determination of gas molecular weight, was obtained during particulate sampling.

During testing, boiler 4 was operated at an output capacity of 100,000 pounds of steam per hour. Boiler operating logs for 12 June and 14 June are provided in Appendix D. These logs indicate hourly steam output and other operating parameters. One of the three runs which comprised a complete test included a soot blow; this is indicated on the field test data sheets provided in Appendixes E-F. Acetone (used for washing the probe liner and nozzle after collecting a sample) blank sample results are provided in Appendix G. Equipment calibration data are found in Appendix H.

Emission calculations were done using "Source Test Calculation and Check Programs for Hewlett-Packard 41 Calculators" (EPA-340/1-85-018) developed by the EPA Office of Air Quality Planning and Standards, Research Triangle Park NC. This is our standard method for calculating emissions data. Emissions calculations are found in Appendix I.

Method 9 determinations for opacity were accomplished during each sample run by a certified test team member. Method 9 field observation forms are provided in Appendixes F and G. EPA Method 9 certification documentation is provided in Appendix J.

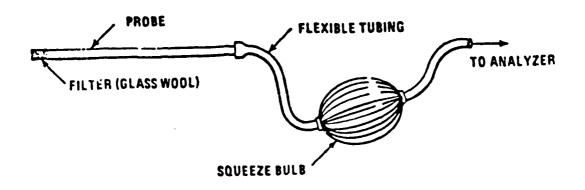
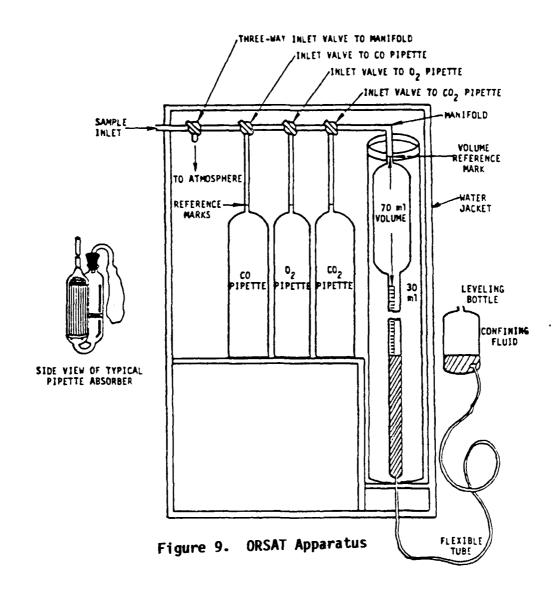


Figure 8. ORSAT Sampling Train



#### III. CONCLUSIONS

Source testing of boiler 4 was conducted on 12 and 14 June 89. Test results for 12 June 89 indicated:

- 1. Visible emissions averaged less than 10% for all runs except for time periods where soot blows occurred. Soot blows did cause opacity to exceed an average of 20% but not for more than a three-minute period.
- 2. Particulate emissions were above the emissions standard of 0.1 grains per dry standard cubic foot (gdscf) with an average value of 0.11 gdscf.

Operational parameters of boiler 4 were adjusted and the unit retested on 14 June. Test results indicated:

- 1. Visible emissions averaged less than 10% for all runs except for time periods where soot blows occurred. Soot blows did cause opacity to exceed an average of 20% but not for more than a three-minute period.
- 2. Particulate emissions were in compliance with applicable standards with an average value of 0.09 gdscf.

The following table provides operating parameters and resultant particulate emission rates determined for each sample run for boiler 4:

#### STACK EMISSION TEST RESULTS

Date	Boiler No.	Run No.	Boiler Operating Capacity (1000 lbs steam/hr)	Soot Blow	Particulate Emissions (gr/dscf)*
12 Jun 89	4	1	100		0.15
12 Jun 89	4	2	100	X	0.09
12 Jun 89	4	3	100		0.09
				Ave	rage 0.11
14 Jun 89	4	1	100	X	0.11
14 Jun 89	4	2	100		0.08
14 Jun 89	4	3	100		0.09
				Ave	rage 0.09

<sup>\*</sup> gr/dscf = grains per dry standard cubic foot

Test results indicate that the Eielson AFB Central Heat and Power Plant is now in compliance with applicable ADEC visible and particulate emissions regulations while operating the boilers at an output capacity of 100,000 pounds of steam per hour.

#### IV. RECOMMENDATION

AFOEHL will remain active in providing Eielson AFB with consultative and field support with regards to the Central Heat and Power Plant.

#### REFERENCES

- "Standards of Performance for New Stationary Sources", Title 40, Part 60, Code of Federal Regulations, July 1, 1987.
- 2. Quality Assurance Handbook for Air Pollution Measurement Systems Volume III, Stationary Source Specific Methods, U.S. Environmental Protection Agency, EPA-600/4-77-027-b, Research Triangle Park, North Carolina, December 1984.
- 3. Source Test Calculation and Check Programs for Hewlett-Packard 41 Calculators. U.S. Environmental Protection Agency, EPA-340/1-85-018, Research Triangle Park, North Carolina, May 1987.

APPENDIX A
Personnel Information

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#### 1. AFOEHL Test Team

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Maj James Garrison, Chief, Air Quality Function

Capt Paul Scott, Consultant, Air Resources Meteorologist

Capt Ronald Vaughn, Consultant, Air Quality Engineer

1LT Charles Attebery, Consultant, Air Quality Engineer

SGT Robert Davis, Environmental Engineering Technician

AFOEHL/ECQ Brooks AFB TX 78235-5501

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#### 2. Eielson AFB on-site representatives

1Lt Clinton Stuart, 343 Medical Group/SGPB SSgt John Willey, 343 Medical Group/SGPB

Ted W. Tisdale 343 CES/DEMP

Utilities Operations General Foreman, Central Heat and Power

Plant

George Pousche 343 CES/DEMP

Assistant, Utilities Operations General Foreman, Central Heat

and Power Plant

Brent Koenen 343 CES/DEEV

Larry Bright 343 CES/DEEV

Jack Coutts Regional Air Coordinator/Dept

of Environmental Conservation.

State of Alaska (phone contact)

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APPENDIX B
Permit No. 8831-AA001

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# STATE OF ALASKA

DEPT. OF ENVIRONMENTAL CONSERVATION

January 21, 1988

SIEVE COWPER, GOVERNOR

(907) 452-1714

Northern Regional Office 1001 Noble Street Suite 350 Fairbanks, Alaska 99701

CERTIFIED MAIL RETURN RECEIPT REOUESTED

Captain George A. Heiner Chief, Environmental/Contract Planning U.S. Department of the Air Force 343D Civil Engineer Squad (AAC) Eielson AFB, Alaska 99702

Dear Capt. Heiner:

Re: Air Quality Control Permit to Operate 8831-AA001

We have received your letter dated January 7, 1988, requesting renewal of Air Quality Control Permit to Operate 8331-AA001. In our review of the permit file, we find a letter dated March 11, 1986 from Capt. Blackshear in which he states "a source test will be conducted after repair. . ." Your letter indicated that the repairs were completed last summer. Since the source test has not been completed, we are requiring it as condition 4 of the new Air Quality Control Permit to Operate #8831-AA001. Please note that the source test report must be submitted to the department by December 31, 1989. The source test will determine at which maximum load the boiler can be fired.

The new permit expires on <u>January 30, 1993</u>, and you must have it renewed if you intend to continue to operate the facility beyond that date. Please note that there are 11 conditions to be met on this permit. Failure to comply with any of these conditions will result in the suspension or revocation of your permit in accordance with 18 AAC 50.310.

Any person who disagrees with this decision may appeal the decision by requesting an adjudicatory hearing, using the procedures contained in 18 AAC 15.200-3:10. Hearing requests must be delivered to the Commissioner of the Department of Environmental Conservation, 3220 Hospital Drive, P.O. Box O, Juneau, Alaska 99811-1800, within 30 days of receipt of this letter. If a hearing is not requested within 30 days, the right to appeal is waived and the decision becomes final.

Sincerely,

William D. McGee

Regional Environmental Supervisor

jc/wdm/tss Enclosure

cc: A. Ewing, EPA/Anchorage

R. Joy, FNSB/Fairbanks

L. Verrelli, ADEC/Juneau

100.16.002

# ALASKA DEPARTMENT OF ENVIRONMENTAL CONSERVATION NORTHERN REGION OFFICE 1001 NOBLE STREET, SUITE 350 FAIRBANKS, ALASKA 99701

#### AIR QUALITY CONTROL PERMIT TO OPERATE

Permit No. 8831-AA001 Renews Permit No. 8331-AA001; Date of Issue January 21, 1988

The Department of Environmental Conservation, under the authority of AS 46.03 and 18 AAC 50.400, issues an Air Quality Control Permit to Operate to:

U.S. Department of the Air Force 343D Civil Engineering Squadron (AAC) Eielson A.F.B., Alaska 99702

FOR THE OPERATION OF the Eielson Air Force Base power and heating plant, consisting of six coal-fired boilers, as described in Exhibit A in accordance with the conditions of this permit and Exhibits A and B and as described in permit application documents listed in Exhibit C.

LOCATED near Fairbanks, Alaska on Eielson Air Force Base.

THE FOLLOWING CONDITIONS SHALL APPLY TO THIS PERMIT:

- 01. The permittee shall comply with the State Ambient Air Quality Standards established in Section 020 and the applicable emission limitation specified in Section 040 of the State Air Quality Control Regulations 18 AAC 50 and Exhibit B.
- 02. An Air Contaminant Emission Source Operating Report as described in Exhibit A shall be submitted semiannually to the department's Northern Regional Office, 1001 Noble Street, Suite 350, Fairbanks, Alaska 99701, by the 30th of January and July of each year.
- 03. The permittee shall maintain and operate all fuel burning equipment, emission control devices, testing equipment, and monitoring equipment to provide optimum fuel burning efficiency during all operating periods. The permittee shall establish and have in the control room written standard operating procedures for use by the operators of the boilers.
- 04. The permittee shall conduct a source test of one representative boiler in accordance with Title 40 Code of Federal Regulation Part 60 Appendix A, Methods 1 through 5 to determine the maximum steam load at which the boilers will meet the emission standards in Exhibit B. The source



#### Permit 8831-AA001 Page 2 of 6

test report must be in the format specified by Appendix IV-3 of the State Air Quality Control Plan and be submitted to the Department's Northern Regional Office by December 31, 1989.

- 05. Until the source test in Condition 4 is conducted, permittee shall operate the coal fired boilers at a firing rate, which at no time shall exceed 100,000 lbs/hr stream, (5/6) rated capacity, based on one-hour average steam production. The source test shall thereafter determine the maximum load.
- 06. Additional testing or monitoring, as deemed necessary, shall be conducted, installed, maintained, and operated in accordance with 18 AAC 50.500 and 50.520 to measure air contaminant emission concentrations. If any continuous monitor is malfunctioning or non-operable for three or more consecutive days, permittee shall notify the Northern Regional Office of the department on the fourth day indicating the cause of failure and anticipated time required to repair the instrument.
- 07. The permittee shall maintain test results, monitoring instrument recording charts, and other applicable data in an active file for not less than one year, and have them accessible, upon request, to the department for not less than three years.
- O8. Permittee shall notify the department's Northern Regional Office by telephone (452-1714) when equipment failures or operation conditions occur which increase air contaminant emissions. Opacity violations totaling less than one-half hour per day do not need to be reported. The permittee shall report the expected duration, nature of occurrence, amount and type of material burned, and steps taken to minimize emissions and avoid recurrence.
- 09. Permittee shall submit a written report by the 15th day of each month to the department's Northern Regional Office which summarizes the date, time, and other information requested in Condition 8 for each incident reported in accordance with that permit condition and in violation of performance limitations listed in Exhibit B.
- 10. The department's representative is allowed access to permittee's facilities to conduct inspections or tests to determine compliance with this permit and state environmental laws and regulations.

#### Permit 8831-AA001 Page 3 of 6

11. A copy of this permit shall be clearly displayed, and the State Air Quality Control Regulations 18 AAC 50 kept on file, at the permitted facility location.

This permit expires 30 January 1993 and may be suspended or revoked in accordance with 18 AAC 50.310.

William D. McGee

Regional Environmental Supervisor

Permit 8831-AA001 Page 4 of 6

### EXHIBIT A AIR QUALITY CONTROL PERMIT TO OPERATE 8831-AA001 AIR EMISSION SOURCE OPERATING REPORT

An Air Source Operating Emission Report shall be submitted to the Alaska Department of Environmental Conservation, Northern Regional Office, 1001 Noble Street, Suite 350, Fairbanks, Alaska 99701 semiannually by January 30 and July 30 each year. The report shall include, but not be limited to, the following information:

- 1. Facility identification and reporting period. Include the firm name, facility name and location, permit number and the period of time covered by the report.
- 2. Operating time and fuel consumption logged on permitted equipment tabulated by quarter. Include the number of days or hours of operation and quantity of fuel consumed by each boiler.
- Report a change in type of fuel and tests or analyses performed.
- 4. A brief discussion of any change in monitoring equipment or failure which may affect reported results or yield incomplete data for any given day.
- 5. Signature of authorized agent preceded by the statement, "I am familiar with the information contained in this report and that to the best of my knowledge and belief such information is true, complete, and accurate."

Permit 8831-AA001 Page 5 of 6

## EXHIBIT B AIR QUALITY CONTROL PERMIT TO OPERATE 8831-AA001 AIR CONTAMINANT EMISSION LIMITATIONS

Exhaust conditions shall be in accordance with the information submitted.

Pollutant	Performance Limitation	Annual Limit TPY
Particulate matter	0.1 grains per dry standard cubic foot, 100,000 lbs steam/hour for each of the 134 MMBTU/HR boilers  20 percent opacity not to be exceeded for more than 3 minutes in any one hour, except during upsets, startups, and shutdowns	150 per each of the six boilers

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#### Permit 8831-AA001 Page 6 of 6

### EXHIBIT C AIR QUALITY CONTROL PERMIT TO OPERATE 8831-AA001 PERMITTEE'S DOCUMENTATION

- 1. Department of the Air Force Air Quality Control Permit to Operate application dated December 19, 1977, and emissions information report OMB 158-R75, dated February 2, 1976.
- 2. The Alaska Department of Environmental Conservation (ADEC) report of "Particulate Matter and Sulfur Dioxide Emissions Source Test" for Eielson Air Force Base's power plant May 14 and 15, 1981.
- 3. ÀDEC letter to U.S. Air Force Director, Engineering Energy and Environmental Planning Elmendorf Air Force Base, dated March 19, 1985, requesting a source test at the Eielson power plant.
- 4. U.S. Air Force letter dated March 11, 1986, to ADEC stating "a source test will be conducted. . ."
- 5. U.S. Air Force letter dated January 7, 1988, to ADEC requesting renewal of Eielson's Air Quality Control Permit to Operate.

APPENDIX C State Regulations

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#### ALASKA AIR QUALITY CONTROL REGULATIONS

(Alaska Administrative Code, Title 18, Environmental Conservation, Chapter 50 — Air Quality Control; Effective May 26, 1972; Amended November 9, 1972; May 8, 1974; May 4, 1980; November 1, 1982; October 30, 1983; June 7, 1987)

# ARTICLE 1. PROGRAM STANDARDS AND LIMITATIONS

50.010. APPLICABILITY OF LOCAL GOVERNMENT REGULATIONS. A local air quality control agency may establish the same or more stringent regulations, but not less stringent regulations, as the applicable regulations specified in this chapter.

50.020. AMBIENT AIR QUALITY STANDARDS. (a) The concentration of contaminants in the ambient air, corrected to standard conditions, may not exceed the following:

- (1) suspended particulate matter -
- (A) annual geometric mean of 60 micrograms per cubic meter; or
- (B) 24-hour average of 150 micrograms per cubic meter more than once each year;
- (2) sulfur oxides, measured as sulfur dioxide —
- (A) annual arithmetic mean of 80 micrograms per cubic meter;
- (B) 24-hour average of 365 micrograms per cubic meter more than once each year; or
- (C) three-hour average of 1300 micrograms per cubic meter more than once each year;
  - (3) carbon monoxide —
- (A) eight-hour average of 10 milligrams per cubic meter more than once each year; or
- (B) one-hour average of 40 milligrams per cubic meter more than once each year;
- (4) ozone one-hour average of 235 micrograms per cubic meter expected more than once per year;

- (5) nitrogen dioxide annual arithmetic mean of 100 micrograms per cubic meter:
- (6) reduced sulfur compounds, expressed as sulfur dioxide 30-minute average of 50 micrograms per cubic meter more than once each year; and
- (7) lead quarterly arithmetic mean of 1.5 micrograms per cubic meter.
- (b) In areas where concentrations of contaminants in the ambient air are less than the standards set out in (a) of this section, the concentrations must be kept below those standards, and no increase above the baseline concentration may exceed
  - (1) for a Class I area
  - (A) suspended particulate matter —
- (i) annual geometric mean of five micrograms per cubic meter; or
- (ii) 24-hour average of 10 micrograms per cubic meter more than once each year; and
- (B) sulfur dioxide ---
- (i) annual arithmetic mean of two micrograms per cubic meter;
- (ii) 24-hour average of five micrograms per cubic meter more than once each year; or
- (iii) three-hour maximum of 25 micrograms per cubic meter more than once each year;
  - (2) for a Class II area
  - (A) particulate matter -
- (i) annual geometric mean of 19 micrograms per cubic meter, or
- (ii) 24-hour average of 37 micrograms per cubic meter more than once each year; and
  - (B) sulfur dioxide -
  - (i) annual arithmetic mean of 20 micro-

grams per cubic meter.

- (ii) 24-hour average of 91 micrograms per cubic meter more than once each year; or
- (iii) three-hour average of 512 micrograms per cubic meter more than once each year;
  - (3) for a Class III area
  - (A) particulate matter
- (i) annual geometric mean of 37 micrograms per cubic meter; or
- (ii) 24-hour average of 75 micrograms per cubic meter more than once each year; and
  - (B) sulfur dioxide
- (i) annual arithmetic mean of 40 micrograms per cubic meter;
- (ii) 24-hour average of 182 micrograms per cubic meter more than once each year:
- (iii) three-hour average of 700 micrograms per cubic meter more than once each year.

50.021. STATE AIR QUALITY CLAS-SIFICATIONS. (a) For purposes of classifying areas according to air quality, those areas in nonattainment with the ambient air quality standards of this chapter are

- (1) Anchorage urban area for carbon monoxide; and
- (2) Fairbanks and North Pole urban areas for carbon monoxide.
- (b) For purposes of the ambient air quality standards specified in 18 AAC 50.020(b)
  - (1) Class I areas in the state are
- (A) Denali (Mt. McKinley) National Park:
- (B) that portion of Bering Sea National Wildlife Refuge designated as a National Wilderness Area;

- (C) that portion of Simeonof National Wildlife Refuge designated as a National Wilderness Area; and
- (D) that portion of Tuxedni National Wildlife Refuge designated as a National Wilderness Area;
- (2) those areas of the state not classified in (a) of this section, or (1) or (3) of this subsection are classified as Class II; and
- (3) no areas in the state have been classified as Class III.
- (c) For purposes of preventing impairment of visibility, the designated areas are
- (1) Mt. Deborah and the Alaska Range East, as viewed from approximately the Savage River Campground area;
- (2) Mt. McKinley, Alaska Range, and the Interior Lowlands, as viewed from the vicinity of Wonder Lake; and
- (3) the Class I areas listed in (b)(1) of this section.
- (d) For purposes of maintaining the ambient air quality standards set out in 18 AAC 50.020(a), the Mendenhall Valley of Juneau is a wood smoke control area.
- 50.030. OPEN BURNING. (a) Open burning must achieve maximum combustion efficiency throughout the burning period, and is subject to the exception in (e) of this section, the limitations in (b), (c), (d), and (f) of this section, and 18 AAC 50.110.
- (b) Open burning of asphalts, rubber products, plastics, tars, oils, oily wastes, contaminated oil cleanup materials, or other materials in a way that gives off black smoke is prohibited without written approval from the department. Approved open burning is subject to the following limitations:
- (1) controlled fires for training fire fighters must be advertised through news media in the general area of the activity at least three days before the activity, informing the public of the time, place, and purpose of the fire, unless waived by the department;
- (2) open burning of liquid hydrocarbons produced during oil or gas well flow tests will be approved only if there are no practical means available to recycle, reuse, or dispose of the fluids in a more environmentally acceptable way; and

- (3) reasonable procedures and requirements must be established by the person doing the burning to minimize adverse environment effects and limit the amount of smoke generated.
- (c) Open burning or incineration of pesticides, halogenated organic compounds, cyanic compounds, or polyurethane products in a way that gives off toxic or acidic gases or particulate matter is prohibted.
- (d) Open burning of putrescible garbage, animal carcasses, or petroleumbased materials is prohibited if it causes order or black smoke which has an adverse effect on nearby persons or residences.
- (e) Controlled burning for the management of forest land, vegetative cover, fisheries, or wildlife habitat, other than burning to combat a natural wildfire, requires written approval from the department.
- (f) Open burning is prohibited in an area if an air quality advisory by the department is broadcast on radio or television stating that burning is not permitted in that area for that day. This advisory will be based on a determination that there is or is likely to be inadequate air ventilation to maintain the standards set by 18 AAC 50.020.
- (g) Open burning is prohibited in wood smoke control areas identified in 18 AAC 50.021(d) between November 1 and March 31.
- 50.040. INCINERATORS. (a) Visible emissions, excluding condensed water vapor, from an incinerator may not reduce visibility through the exhaust effluent by
- (1) greater than 20 percent for a total of more than three minutes in any one hour, except as provided in (2) of this subsection; or
- (2) 20 percent or greater for municipal wastewater treatment plant sludge incinerators.
- (b) Emissions of particulate matter from incinerators may not exceed, per cubic foot of exhaust gas corrected to 12 percent CO, and standard conditions, and except as specified in (c) of this section
- (1) 0.15 grains for incinerators less than 2,000 pounds, but greater than or equal to 1,000 pounds per hour rated capacity; or
- (2) 0.08 grains from incinerators of 2,000 pounds per hour rated capacity or larger.

- (c) Emissions of particulate matter from municipal wastewater treatment plant sludge incinerators which serve 10,000 or more persons and burn waste containing more than 10 percent wastewater treatment plant sludge by dry weight, may not exceed 0.65 grams per kilogram of dry sludge input.
- 50.050 INDUSTRIAL PROCESSES AND FUEL BURNING EQUIPMENT.
  (a) Visible emissions, excluding condensed water vapor, from an industrial process or fuel burning equipment may not reduce visibility through the exhaust effluent by
- (1) greater than 20 percent for a total of more than three minutes in any one hour, except as noted in (2) (8) of this subsection:
- (2) greater than 30 percent for more than three minutes in any one hour for fuel burning equipment in operation before November 1, 1982 and using more than 20 percent woodwaste as fuel;
- (3) greater than 30 percent for urea prilling towers in operation before July 1, 1972, for a total of more than three minutes in any one hour;
- (4) 20 percent or greater for asphalt plants installed or modified after November 1, 1982:
- (5) 20 percent or greater for process emission: other than from pneumatic cleaners, at coal preparation facilities installed or modified after November 1, 1982:
- (6) 10 percent or greater for pneumatic cleaners at coal preparation facilities installed or modified after November 1, 1982.
- (7) 10 percent or greater for process emissions, other than from kilns, at portland cement plants installed or modified after November 1, 1982; and
- (8) 20 percent or greater for kilns at portland cement plants installed or modified after November 1, 1982.
- (b) Particulate matter emitted from industrial processes or fuel burning equipment may not exceed, per cubic foot of exhaust gas corrected to standard conditions
- (1) 0.05 grains except as provided in (2) (4) of this subsection, (d) of this section, and 18 AAC 50.060;
- (2) 0.1 grains for steam generating plants burning as fuel

- (A) coal, and in operation before July 1, 1972;
- (B) coal, and rated less than 250 million Btu per hour heat input; or
  - (C) municipal wastes;
  - (3) 0.1 grains for an industrial process in operation before July 1, 1972; or
  - (4) 0.15 grains from fuel burning equipment in operation before November 1, 1982, and using more than 20 percent woodwastes as fuel.
  - (c) Sulfur compound emissions, expressed as sulfur dioxide, from an industrial processs or from fuel burning equipment may not exceed 500 ppm averaged over a period of three hours, except as provided in (d) of this section, and 18 AAC 50.060.
  - (d) Emissions from a source installed or modified after November 1, 1982 may not exceed
  - (1) at asphalt plants, 90 milligrams of particulate matter per cubic meter of exhaust gas at standard conditions;
    - (2) at petroleum refineries
  - (A) catalytic cracking unit catalyst regenerator
  - (i) 1.0 kilogram of particulate matter per 1,000 kilograms of coke burnoff;
  - (ii) 43.0 additional grams of particulate matter per million joules supplemental heat attributable to fuels burned in a catalyst regenerator waste heat boiler; and
  - (iii) 500 ppm carbon monoxide by volume of exhaust gas;
  - (B) suffur recovery plant rated at more than 20 long tons per day
  - (i) 250 ppm sulfur dioxide at zero percent oxygen on a dry basis; or
  - (ii) 10 ppm hydrogen sulfide and a total of 300 ppm reduced sulfur compounds, expressed as sulfur dioxide, at zero percent oxygen on a dry basis, if the air contaminants are not oxidized before release to the atmosphere; and
  - (C) fuel burning equipment, sulfur dioxide averaged over three hours
  - (i) equal to the concentration of uncontrolled emissions which would result from burning fuel gas containing 230 milligrams hydrogen sulfide per dry standard cubic meter from equipment burning fuel
  - (ii) a calculated concentration based on the allowable emissions in (i) and (iii) of this subparagraph and the proportion of

- fuel gas and other fuels to the total fuel burned in fuel burning equipment; or
- (iii) 500 ppm from all other fuel burning equipment;
  - (3) at coal preparation facilities
- (A) thermal drying unit, 70 milligrams of particulate matter per cubic meter of exhaust gas at standard conditions; and
- (B) pneumatic coal cleaning unit, 40 milligrams of particulate matter per cubic meter of exhaust gas at standard conditions; and
  - (4) at portland cement plants
- (A) clinker cooler, 0.050 kilograms of particulate matter per 1000 kilograms of feed on a dry basis to the kiln; and
- (B) kiln, 0.15 kilograms of particulate matter per 1000 kilograms of feed on a dry basis.
- (e) Release of materials other than process emissions, products of combustion, or materials introduced to control pollutant emissions from a stack at a source built or modified after November 1, 1982 is prohibited unless approved in writing by the department.
- (f) No person may cause or permit bulk materials to be handled, transported, or stored, or engage in an industrial activity or construction project without taking reasonable precautions to prevent particulate matter from becoming airborne.
- 50.060. PULP MILLS. Average emissions per ton of pulp produced from a sulfite pulp mill may not exceed in any 24-hour period
- (1) 20 pounds of sulfur oxides (expressed as sulfur dioxide) from blow pits, washer vents, storage tanks, digester relief systems, and recovery systems; and
- (2) two pounds of particulate matter from blow pits, washer vents, storage tanks, digester relief systems, and recovery systems.
- 50.070. MOTOR VEHICLE EMISSIONS. (a) Emissions from gasoline-powered motor vehicles, excluding condensed water vapor, may not be visible for more than any five consecutive seconds.
- (b) Visible emissions from dieselpowered motor vehicles, excluding condensed water vapor, may not result in a reduction of visibility of greater than 40 percent through the exhaust effluent for more than any five consecutive seconds.

- 50.080. [Repealed]
- 50.085. WOOD-FIRED HEATING DEVICES. For wood-fired heating devices,
- (1) when an air quality alert is issued under 18 AAC 50.610(a)(1)(B) for particulate matter within a specific area, except areas set out in (3) of this section, visible emissions at the point of release to the atmosphere may not reduce visibility through the exhaust effluent by 50 percent or greater for more than 15 minutes in any one hour;
- (2) burning in a way that creates black smoke is prohibited; and
- (3) for wood smoke control areas identified in 18 AAC 50.021(d)
- (A) visible emissions at the point of release to the atmosphere may not reduce visibility through the exhaust effluent by 50 percent or greater for more than 15 minutes in any one hour; and
- (B) when an air emergency has been issued under 18 AAC 50.610 (a)(3)(D), no person may operate, permit, or allow the operation of a wood-fired heating device which results in the emission of smoke.
- 50.090. ICE FOG LIMITATIONS. The department will, in its discretion, require any person proposing to build or operate an industrial process, fuel burning equipment or incinerator in areas of potential ice fog, to obtain a permit to operate and to reduce water emissions.
- 50.100. MARINE VESSELS. Within three miles of the coastline of Alaska, visible emissions from any marine vessel, excluding condensed water vapor, may not result in a reduction of visibility through the exhaust effluent of greater than
- (1) 40 percent for a period or periods aggregating more than three minutes in any one hour, except as provided in (2) of this section; and
- (2) 40 percent for a period or periods aggregating more than six minutes in any one hour during initial startup of diesel-driven vessels.
- 50.110. AIR POLLUTION PROHIBITED. No person may permit any emission which is injurious to human health or welfare, animal or plant life, or property, or which would unreasonably interfere with the enjoyment of life or property.

50.120 - 50.190. [Repealed]

### ARTICLE 2. PERMIT REQUIREMENTS

50.300. PERMIT TO OPERATE. (a) No person may construct, modify, reconstruct, operate, or cause the operation of the following without a permit from the department:

(1) a facility containing a source which requires an air contaminant emission control unit or system to comply with emission standards set by 18 AAC 50.040—18 AAC 50.060, and which is

(A) an industrial process with a total design rate, capacity, or throughput greater than five tons per hour and which physically or chemically treats the material; or

(B) fuel-burning equipment with a rating of 50 million Btu per hour or greater;

(2) fuel-burning equipment with a rating of 100 million Btu per hour or more;

(3) an incinerator with a rated capacity of 1,000 pounds per hour or more;

(4) a facility subject to the standards set by 18 AAC 50.040(c), 18 AAC 50.050(a)(5), 18 AAC 50.050(a)(7), or 18 AAC 50.050(d);

(5) a facility

(A) which has allowable emissions of 100 tons per year or more of an air contaminant regulated under the Clean Air Act (P.L. 91-604) as amended August 7, 1977 (P.L. 95-95), is installed after November 1, 1982, and is a

(i) fossil fuel fired steam electric plant of more than 250 million Btu's per hour heat input:

(ii) coal cleaning plant (with thermal dryers);

(iii) kraft pulp mill;

(iv) portland cement plant;

(v) primary zinc smelter;

(vi) iron and steel mill plant;

(vii) primary aluminum ore reduction plant;

(viii) primary copper smelter;

(ix) municipal incinerator capable of charging more than 250 tons of refuse per day;

(x) hydrofluoric, sulfuric, or nitric acid plant;

(xi) petroleum refinery;

(xii) lime plant;

(xiii) phosphate rock processing plant;

(xiv) coke oven battery;

(xv) sulfur recovery plant;

(xvi) carbon black plant (furnace process);

(xvi!) primary lead smelter;

(xviii) fuel conversion plant;

(xix) sintering plant;

(xx) secondary metal production plant;

(xxi) chemical process plant;

(xxii) fossil fuel boiler or a combination of boilers totaling more than 250 million Btu's per hour heat input;

(xxiii) petroleum storage and transfer unit with a total storage capacity exceeding 300,000 barrels;

(xxiv) taconite ore processing plant;

(xxv) glass fiber processing plant; or

(xxvi) charcoal production plant;

(B) which is listed in (A) of this paragraph with allowable emissions of less than 100 tons per year of a regulated air contaminant and is modified after August 7, 1977, causing an increase in allowable emissions of 100 tons per year or more; or

(C) which is listed in (A) of this paragraph with allowable emissions of greater than 100 tons per year of a regulated air contaminant and is modified after August 7, 1980, or after the date of the most recent permit issued for the affected area under 18 AAC 50.400(c)(3), causing an increase in actual emissions equal to or exceeding the emissions listed in (6)(C)(i)—(xvii) of this subsection;

(6) a facility not listed in (5) of this subsection

(A) which has allowable emissions of 250 tons per year or more of an air contaminant regulated under the Clean Air Act (P.L. 91-604) as amended August 7, 1977 (P.L. 95-95), and is installed after November 1, 1982;

(B) which has allowable emissions of less than 250 tons per year of a regulated air contaminant and is modified after August 7, 1977, causing an increase in allowable emissions of 250 tons per year or more; or

(C) which has allowable emissions of more than 250 tons per year of a regulated air contaminant and is modified after August 7, 1980, or after the date of the most recent permit issued for the affected area under 18 AAC 50.400(c)(3), causing an increase in actual emissions equal to exceeding any of the following:

(i) carbon monoxide - 100 tpy;

(ii) nitrogen oxides - 40 tpy;

(iii) sulfur dioxide — 40 tpy;

(iv) particulate matter - 25 tpy;

(v) ozone — 40 tpy of volatile organic compounds as an ozone indicator;

(vi) lead — 0.6 tpy;

(vii) asbestos — 0.007 tpy;

(viii) beryllium — 0.0004 tpy;

(ix) mercury — 0.1 tpy;

(x) vinyl chloride — 1 tpy;

(xi) fluorides — 3 tpy;

(xii) sulfuric acid mist — 7 tpy;

(xiii) hydrogen sulfide (H,S) - 10 tpy;

(xiv) total reduced sulfur including H<sub>2</sub>S — 10 tpy;

(xv) reduced sulfur compounds including H<sub>2</sub>S — 10 tpy;

(xvi) increased emissions of a pollutant regulated by the Clean Air Act (PL 91-604) as amended August 7, 1977 (PL 95-95) and not listed in (6)(C)(i)-(xv) of this subsection; or

(xvii) notwithstanding (i) through (xvi), if located within 10 kilometers of an area listed in 18 AAC 50.021(b)(1) with increased emissions that impact the area by 1 ug/m<sup>3</sup> or more for a 24-hour average;

(7) a source or facility installed, reconstructed, or modified after July 1, 1979 or after the date of the most recent permit issued since November 1, 1982, under 18 AAC 50.400(c)(4), located within an area identified in 18 AAC 50.021(a), and causing an increase in actual or allowable carbon monoxide emissions, whichever is greater, from the source or facility of 100 tons per year or more; or

(8) a facility or modification to a facility for which the owner or operator has requested that the department approve limitations of emission rates or operations to reduce emissions to levels below those specified in this chapter.

(b) An application for a permit required by (a) of this section must include

(1) one set of plans and specifications clearly showing the layout of the proposed facility, location of individual equipment and points of discharge, building dimensions, and stack heights;

(2) a map or aerial photograph, on a scale at least one inch to one mile indicating the location of the proposed facility, homes, buildings, roads, and other adjacent facilities, and the general topography within 15 kilometers of the facility;

(3) an engineering report outlining the proposed methods of operation, the

amount of material to be processed, the proposed use and distribution of the processed material, and a process flow diagram with description showing points of emission and estimated amounts and types of air contaminants to be emitted:

(4) a description of air quality control devices, including efficiency and other design criteria, and assurances that this equipment is capable of complying with applicable emission requirements specified in this chapter:

(5) if requested by the department, an evaluation of the effect of the facility's expected maximum emissions on the ambient air, including ambient air quality and meterorological data;

(6) if requested by the department, plans for emission reduction procedures to be used during an air episode; and

(7) a detailed schedule for construction or modification of the facility.

- (c) A permit application for a facility subject to (a)(5) or (a)(6) of this section must include the following information in addition to that required under (b) of this section:
- (1) ambient air and meteorological data to fully describe the air quality in the vicinity of the proposed facility and any changes in air quality due to general growth which has occurred after the establishment of the baseline date in the area the facility or modification would affect; department approval of the air monitoring network is required before starting data collection;
- (2) a detailed demonstration that the expected maximum emissions from the construction and operation of the facility, including emissions from associated growth, will not cause a violation, or contribute to an existing violation, of the ambient air quality standards in 18 AAC 50.020(a) or allowable increments in 18 AAC 50.020(b);
- (3) an adequate demonstration that the proposed emission control system represents the best available control technology for each air contaminant and for each new or modified source; and
- (4) an analysis of the impact of expect-

including emissions from associated growth, on visibility, vegetation, and soils.

- (d) A permit application for a facility subject to (a)(7) of this section must include the following information in addition to that required under (b) of this
- (1) proof that emissions of a pollutant for which the area is declared in nonattainment will not exceed the applicable emission allowance, and will be controlled to a rate which represents the lowest achievable emission rate; and
- (2) proof that other sources owned or operated by the applicant within the state are in compliance with the requirements of this chapter and the Clean Air Act (P.L. 91-604) as amended August 7, 1977 (P.L. 95-95).
- (e) A permit application submitted under (a)(8) of this section need not include the information required under (b) and (c) of this section, but must specify the limitations on emission rates or operations necessary to exempt the facility from 18 AAC 50.300(a)(5) — (7) or any other requirement of this chapter.
- (f) If a permit application is deficient, the department will notify the applicant by certified mail within 30 days after receipt of the application, identifying the deficiencies and the information to be submitted. When the deficiencies are corrected, the department will continue processing the application.

50.310. REVOCATION OR SUSPEN-SION OF PERMIT. A permit to operate will, in the department's discretion, be revoked or suspended if the conditions of the permit or applicable laws or regulations are violated.

#### ARTICLE 3. PERMIT REVIEW CRITERIA

APPLICATION REVIEW 50.400. AND ISSUANCE OF PERMIT TO OP: ERATE. (a) Before review under (b) of this section for a facility described in 18 AAC 50.300(a)(5), (6), or (7); for a facility with a stack described in 18 AAC 50.900(23)(C); or for any other facility for which the department finds that additional public review and comment is desirable, ed maximum emissions from the facility, an opportunity for public comment and hearing will be provided using the following procedures:

- (1) at least 30 days before beginning review under (b) of this section a summary of the decartment's preliminary review and analysis of the application will be published in a newspaper of general circulation within the area where the new or modified facility is to be located. The analysis will be sent to the Environmental Protection Agency, and any federal land manager, Indian governing body on a reservation, or unit of local government which may be affected by emissions from the proposed activity; materials submitted by the applicant and a copy of the proposed permit will be available in at least one location within the area of the new or modified facility;
- (2) the department, upon its own motion, or upon request, will hold a public hearing on the application following the procedures set out in 18 AAC 15.060(d) -(g); 60 days notice of a hearing will be sent to any affected federal land manager under 18 AAC 50.021(c); and
- (3) public comments and testimony received on the application will be evaluated as part of the information needed to complete evaluation of the permit application. and will be made available to the public.
- (b) The department will review a permit application and will, in its discretion, issue the permit within 30 days after receipt of all information needed to complete evaluation of the application, including testimony at a public hearing held under (a) of this section. For applications subject to (a) of this section, a copy of the final determination will be published and distributed as described in (a)(1) of this section.
- (c) The department will issue a permit only if the applicant shows that
- (1) allowable emissions from the facility and from associated growth will not prevent or interfere with the attainment or maintenance of ambient air quality standards set by 18 AAC 50.020(a);
- (2) air contaminant emissions from a source in the facility will not exceed the requirements of 18 AAC 50.040 - 18 AAC 50.060 and 18 AAC 50.110 and are approvable by the Environmental Protec-

tion Agency under the federal new source performance standards or emission standards for hazardous air pollutants;

- (3) for a facility subject to 18 AAC 50.300(a)(5) or (6),
- (A) the best available control technology for controlling emissions of each pollutant will be installed and used for each new or modified source;
- (B) in an area designated in 18 AAC 50.021(b) as in attainment with ambient air quality standards set by 18 AAC 50.020(a), allowable emissions from the facility and from associated growth will not
- (i) cause or contribute to an increase in air contaminants greater than specified in 18 AAC 50.020(b); or
- (ii) cause an increase of carbon monoxide more than 500 ug/m' eight-hour average or 2000 ug/m' one-hour average within any area specified in 18 AAC 50.021(a); and
- (C) allowable emissions from the facility and from associated growth will not adversely affect air quality related values, including noise, odor, visibility, vegetation, and soils of any area within the state; and
- (4) for a facility subject to 18 AAC 50.300(a)(7),
- (A) emissions will not exceed the emission allowance in the applicable nonattainment area;
- (B) the lowest achievable emission rate will be achieved for each new or modified source; and
- (C) other sources owned or operated by the applicant within the state are in compliance with requirements of this chapter and the Clean Air Act (P.L. 91-604) as amended August 7, 1977 (P.L. 95-95).
  - (d) A permit to operate
- (1) will be granted for no more than five years, after which the permit must be renewed for continued operation of the facility;
- (2) will include a compliance schedule if the facility is emitting air contaminants in excess of applicable limitations contained in this chapter, based on the minimum time necessary to install the required control equipment; a permit which includes a compliance schedule must be renewed every year of its duration;
- (3) will, in the department's discretion, require the permittee to install, use, and

- maintain monitoring equipment; to sample emissions according to methods prescribed by the department, at locations and intervals and by procedures specified by the department; to provide source test reports; to provide monitoring data, emission data, and information from analyses of any test samples; and to make periodic reports on process operations and emissions;
- (4) will, for an application submitted under 18 AAC 50.300(a)(8), include specific limitations on emissions or operations as necessary to exempt the facility from 18 AAC 50.300(a)(5) (7) or any other requirement of this chapter;
- (5) will, in the department's discretion, require that specific emission reduction procedures be taken during an air episode; and
- (6) may not be transferred without the written consent of the regional supervisor.
- (e) If an application for a permit is denied, the department will notify the applicant by certified mail, stating the reasons for denial. The notification will include a statement that a person aggrieved by the department's decision may request in adjudicatory hearing within 30 days after service of the denial under 18 AAC 15.200 18 AAC 15.310. For applications subject to (a) of this section, a copy of the final determination will be published and distributed as described in (a)(1) of this section.

50.410. [Repealed]

## ARTICLE 4. REGULATION COMPLIANCE CRITERIA

- 50.500. SOURCE TESTING. (a) Except as provided in (d) of this section, the department will, in its discretion, conduct or have conducted air contaminant emission tests to determine compliance with this chapter.
- (b) Testing to determine compliance with this chapter must be by methods approved by the department and done at a point or points which characterize the actual discharge into the ambient air.
- (c) Except as provided in (d) of this section, air contaminant emission tests must be done at maximum rate burning or operating capacity of the unit, or other

- rate determined by the department to characterize the actual discharge into the ambient air.
- (d) Demonstration by source testing of compliance with the requirements of 18 AAC 50.040(a)(2) and (b)(2) for incinerators greater than 4,100 pounds per hour, 18 ACC 50.050(a)(1) for catalyst cracking unit catalyst regenerators, 18 AAC 50.040(c), 18 AAC 50.050(a)(4) (8) and (d) must be done at maximum operating or production rates within 180 days after startup of a new or modified source. Source test methods specified in 40 CFR 60, Appendix A, as amended through November 1, 1982 or their equivalent are to be used as follows:
- (1) for emissions of particulate matter, procedures specified in reference methods 1, 2, 3, 4, and 5;
- (2) for emission of carbon monoxide, procedures specified in reference method 10:
- (3) for emissions of sulfur dioxide, procedures specified in reference methods 1, 2, and 6;
- (4) for emissions of reduced sulfur compounds, procedures specified in reference method 15:
- (5) for hydrogen sulfide content of process fuel gas streams, procedures specified in reference method 11; and
- (6) for visible emissions, procedures specified in reference method 9.
- (e) If the provisions in (d) of this section do not apply, then compliance with emission standards must be measured by the following:
- (1) for emissions of particulate matter, procedures specified in reference methods 1, 2, 3, 4, and 5 of Appendix A to 40 C.F.R. sec. 60 as amended through November 1, 1983;
- (2) for emissions of sulfur dioxide, procedures specified in reference methods 1, 2, and 6 of Appendix A to 40 C.F.R. sec. 80 as amended through November 1, 1983; and
- (3) to determine the reduction of visibility and opacity of exhaust gases, the procedures specified in the department document entitled "Alaska Air Quality Visible Emissions Evaluation Procedures" (dated August 1983).
- (f) To determine compliance with this chapter, standard exhaust gas volumes

must include only the gases formed from theoretical combustion of the fuel, plus the excess gas volume normal for the specific tain, and operate continuous emission and source type, corrected to standard conditions.

50.510. AMBIENT ANALYSIS METHODS. (a) Air quality data and analyses submitted in support of a permit application under 18 AAC 50.300(a)(5) or (6) must comply with procedures set out in the department document entitled "ADEC Ambient Analysis Procedures" (dated July 1982).

(b) Continuous ambient air monitoring is required in support of a permit application submitted under 18 AAC 50.300(a)(5) or (6) for each pollutant which exceeds the limitations described in 18 AAC 50.300(a)(6)(C)(i) - (xvii) unless the existing concentrations or the predicted ambient air quality impacts are less than

- (1) carbon monoxide 575 ug/m<sup>3</sup>, 8-hour average;
- (2) nitrogen dioxide 14 ug/m3, annual average;
- (3) total suspended particulates -10 ug/m', 24-hour average;
- (4) sulfur dioxide 13 ug/m<sup>3</sup>, 24-hour average:
- (5) ozone -any increase in allowable or actual volatile organic compounds emissions of 100 tons per year or more;
- (6) lead 0.1 ug/m', quarterly average:
- (7) mercury 0.25 ug/m<sup>3</sup>, 24-hour average;
- (8) beryllium 0.001 ug/m<sup>3</sup>, 24-hour average;
- (9) fluorides 0.25 ug/m<sup>3</sup>, 24-hour average:
- (10) vinyl chloride 15 ug/m<sup>3</sup>, 24-hour average; and
- (11) hydrogen sulfide 0.2 ug/m3, 1-hour average.

50.520. EMISSION AND AMBIENT MONITORING, (a) Operators of facilities requiring a permit under 18 AAC 50.300 shall install, maintain, and operate continuous ambient air quality, meteorological, process, or emission monitoring and recording devices specified by the department and in accordance with 40 CFR sec. 58, Appendix B, as amended through November 1, 1983.

(b) Operators of facilities subject to 18

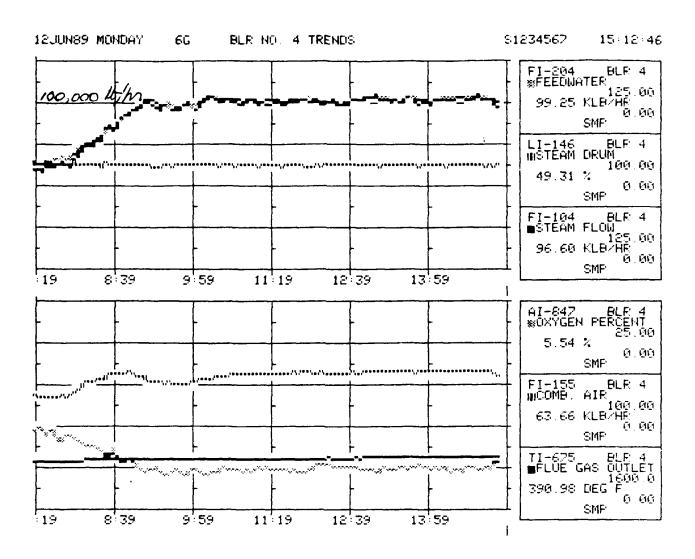
- AAC 50.040(b)(2), 18 AAC 50.040(c), 50.021(b)(1) of this chapter will not be or 18 AAC 50.050(d) shall install, mainprocess monitoring devices, keep records. and report excess emissions in accordance with procedures established in 40 CFR sec. 60 as amended through November 1,
- (c) The department will, in its discretion, require the owner or operator of an air contaminant source to keep records and periodically report on the nature and amount of emissions as necessary to determine compliance with this chapter.
- 50.530. CIRCUMVENTION. (a) Use of air for dilution of emission contaminants without causing a total decrease in the contaminants is not permitted as a method of compliance with this chapter, except that dilution air may be used at sulfur recovery plants with a maximum production rate of 20 long tons per day or less to achieve compliance with the 500 ppm sulfur dioxide requirement in 18 AAC 50.050(c).
- (b) A person owning or operating a facility emitting air contaminants subject to the limitations and provisions of this chapter shall ensure that the facility is in compliance with this chapter and any other applicable local, state, or federal law.
- (c) Stack heights which exceed good engineering practice, or dispersion techniques, may not be used to affect the degree of emission limitation required for control of air contaminants.
- (d) No person may construct, operate, or modify an air contaminant emission source which will result in a violation of the applicable emission standards or will interfere with the attainment or maintenance of the ambient air standards of this chapter.

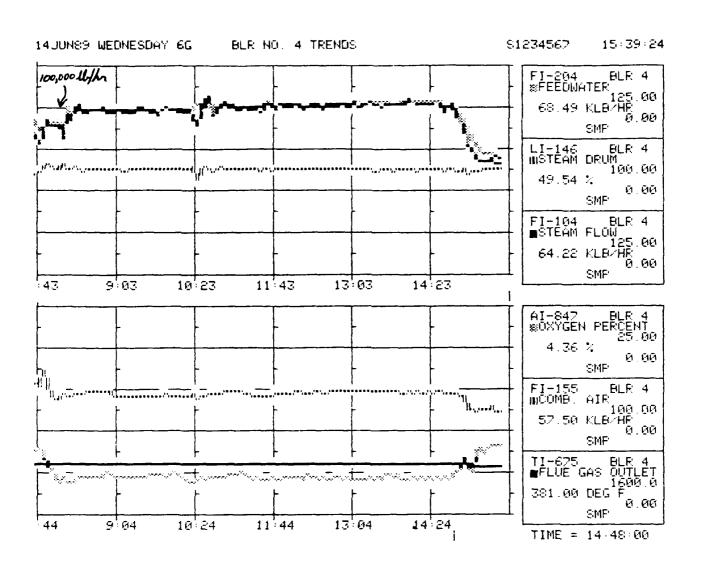
#### ARTICLE 5. PROCEDURAL AND **ADMINISTRATIVE**

50.600. RECLASSIFICATION PROCEDURES AND CRITERIA. (a) The department will, in its discretion, periodically review and revise the air quality classifications within the state after notice and public hearing, except that

- reclassified; and
- (2) the following areas may be reclassified only to Class I or II:
- (A) an area which exceeds 10,000 acres in size and is a national monument, national primitive area, national preserve, national recreation area, national wild and scenic river, national wildlife refuge or range, or national lakeshore or seashore;
- (B) a national park or national wilderness area established after August 7, 1977 which exceeds 10,000 acres; and
- (3) land within the exterior boundaries of reservations of federally recognized Indian tribes may be redesignated only by the appropriate Indian governing body.
- (b) Reclassification will be initiated by the department on its own motion, or upon receipt of a petition for reclassification containing
- (1) detailed reasons why reclassification is requested and is in the best interests of the public:
- (2) an accurate description of the proposed boundaries of the area and the air quality within it;
- (3) a detailed evaluation of emission and ambient air quality effects of any proposed new or modified facility;
- (4) an evaluation of the effects of any proposed new or modified facility on air quality within other areas classified under 18 AAC 50.021;
- (5) a detailed analysis of the health, environmental, economic, social, and energy effects of the proposed reclassification;
- (6) if an area proposed for reclassification includes or is part of a local government jurisdiction
- (A) a resolution recommending reclassification and adopted by each affected unit of local government; and
- (B) evidence that the resolution required under (A) of this paragraph was adopted after public hearing with at least 15 days' prior notice published in a newspaper of general circulation.
- (c) The department will review the petition for reclassification within 30 days after receipt and will accept it for consideration if it satisfactorily describes the circumstances behind the proposed reclas-(1) the areas identified in 18 AAC sification and meets the requirements of

APPENDIX D
Plant Operating Data





APPENDIX E Boiler #4, Field Data, 12 July 89

#### DETERMINATION OF MINIMUM NUMBER OF TRAVERSE POINTS

Stack ID: BOLER #4 Stack diameter at ports: 52

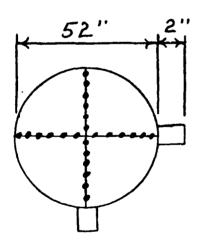
Distance A (ft) // 2" (duct diameters) 2.6

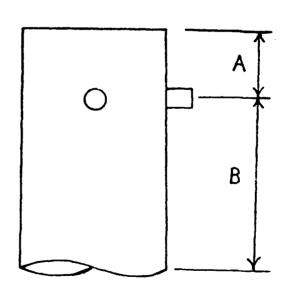
Recommended number of traverse points as determined by distance A: 24

Distance B (ft) 3' (duct diameters) 0.7

Recommended number of traverse points as determined by distance B: 24

Number of traverse points used: 24





1	PR	RELIMINARY SURVEY (Stack Ge		ET NO. 1
BASE EIELSCI	a /	PLANT	01 17N	VT 81 D( 630)
DATE		Į.	1 ~ ///	YT BL-DG-6302
12 JUNE RCE TYPE AND MAKE		AFCEHL		
BOILER H	+4, COA	L MRED	· · · · · · · · · · · · · · · · · · ·	
#4		52"		Inches
RELATED CAPACITY	STEAM/AL		COAL	
12-C 1103 lb	E OF NIPPLE TO IN	NSIDE DIAMETER	CLITT	
NUMBER OF TRAVERSES		NUMBER OF POINTS/TE	RAVERSE	Inches
2		12 OCATION OF SAMPLING P	POINTS ALONG T	TRAVERSE
POINT	PERCENT OF DIAMETER	F DISTANCE F	ROM	TOTAL DISTANCE FROM OUTSIDE OF NIPPLE TO SAMPLING POINT (Inches)
1				3.1
2				5,5
3				8.1
١/				11.2
5				15.0
6				20.5
7				35,5
8				41.0
9				44. 8
10				47. 9
11				50.5
12				52.9
	1		ł	

OEHL FORM 15

		EY DATA SHEET NO. 2 emperature Traverse)	
BOILER NUMBER	7FB	12 JUNE 89	
BOILER NUMBER			
INSIDE STACK DIAMETER	52		Inches
STATION PRESSURE	19 266		In Hg
STACK STATIC PRESSURE	21. 20p	35 Vt	In H20
SAMPLING TEAM AFOEHL			
TRAVERSE POINT NUMBER	VELOCITY HEAD, Vp IN H20	W B	STACK TEMPERATURE (OF)
	0,95	3 16	350
Z	. 1,30	8 16	404
3	1,30	8 14	405
4	1,26	0 2	407
5	1.20	20	407
Ç	1.15	0 3	406
7	1.00	3 10	407
3	1,05	3 12	407
9	0.98	5 13	407
10	0.93	12 10	407
	0.95	15 12	406
12	7.90	10 10 ArG = 8°	406
		ALG = 8°	
	FPS = 69		
	$\widehat{I}_{\zeta} = 1.63$ $\widehat{I}_{\zeta} = 462$		
	Ts = 402		
		Norrel 24	17
		Nozzel 24 actual = . 25	06
	AVERAGE		U

RUN NUMBER	1/1	SCHEM	SCHEWATIC OF STACK CROSS SECTION	ROSS SEC		EQUATIONS	7	,	7	AMBIENT	TEMP 70	90
DATE /2 56	SUNE 89		7	[] meter	tr X	R = F + 460	Fd. Co. A 2	E E		STATION PRESS	1.2	5 & in He
PLANT RIRCOW AWER PLINT	DNT BLTG 6203	(203	8478	•0		S	<del></del> , .	Ts	<	HEATER	HEATER BOX TEMP	
BXSE E1E1.50~	Sort					pitet	pitat to be church	6 - Scoel	रे	PROBE	EATER SETTH	97
SAMPLE BOX NUMBER	UMBER					gaelea	pretrate churk (3) 145	1) ()( 1) 805	<u>.</u>	PROBE LENGTH	FNGTH 72	
METER BOX NUMBER	JMBER		15.5			Orst 0	Ocet Oak chark	s (		NOZZLE	NOZZLE AREA (A) DIH	4
Qw/Qm			2 2 2	n		7 - 53	0 7. C"H"	م ا	<b>≯</b>	Cp	1.8.	
3		1/4/		i						DRY GA	GAS FRACTION (Fd)	G
TRAVERSE	SAMPLING	BILLY 1%	STACK TEMP	$\vdash$	VELOCITY	ORIFICE	GAS	GAS	GAS METER TE	TEMP	SAMPLE	IMPINGE
POINT	TiME (min)	The state of	(oF) (T)	(Ts) (oR)	HEAD (Vp)	OIFF. PRESS. (H)	SAMPLE VOLUME (cu ft)	N (9.6)	AV (Tra) (SE)	OUT (OF)	BOX TEMP (0F)	OUTLET TEMP (OF)
(4)[	Ċ	ぶん	272		14.	41.0	475,55	200		Q	1)(1	12
2	2'1	3.0	400		1.05	69.2		\$2		- 7/4	272	99
4	5.00	0000	00%	+	1.45	2.96		36		31	533	6.5
4	7.5	2,5	tat	7	1,20	3.69		22		82	253	100
4,	0,0	200	1,02	7	37	5.09		16		3/2-	7,57	8 थं
214	15.0	2.5	404	-	22/	3,10		100		\\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\ \\	236	77.5
2	12,5	4.0	704		07'	2 10		90		25	25.2	34
9	20.02	4.6	409		1,5	۱۳.		76		200	253	10
0)	62.1	90	77/		, 15,	66.2.		36		1/3	255	93
//	65.0	4.0	405	+	1.10	2.8%		86		44	757	97
16	4	3.0	762	$\dashv$	, SX	2,19		23		20	2.5.3	24
	2000	200	+	+			54.385			+		
				+					+	+		
										-		
			-	+								
			+	+								
			4	+			_	_	_	_		

PLANT		THE PROPERTY OF THE PARTY OF TH	CAMENTAL ACTION PROPERTY	66.00	1				AMA	AMRIENT TEMP	
# 7			TIC OF STACK C	KOSS SEC		EQUATIONS			C	L E	
7	2/2					$^{\circ}R = ^{\circ}F + 460$	0		STAI	STATION PRESS	90 1
	N F 39	<u> </u>					- 5130. Ed. Co. A 7 2				in Hg
					-	# #	· —	Ts . Vp	HEA	HEATER BOX TEMP	
BASE									PROF	PROBE HEATER SETTING	NG
SAMPLE BOX NUMBER	18ER								PRO	PROBE LENGTH	
			•								ıı
METER BOX NUMBER	BER						•		NOZ	NOZZLE AREA (A)	3
Qw/Qm									ď		al bs
ပိ		14/							ORY	DRY GAS FRACTION (Fd)	(p.
TRAVERSE	SAMPLING	EST ATTEN	I STACK TEM		VELOCITY	ORIFICE	GAS	G GAS METER	[위	3 SAMPLE	I IMPINGER
POINT	TIME (min)	AIN HOO	(oF) (T	(Ts) (oR)	HEAD (Vp)	PRESS.	SAMPLE VOLUME (Qu ft)	N (9.	AVG OUT (Tm) (0F)		/ OUTLET TEMP (OF)
1(8)	0	3 5	552		, 86	2,77	581165	06	-	252	77
2	21.5	4.5	$d\omega$		071	3.65		7.6	88	255	73
~	5.0	4,5	400	+	1,45	3.78		7.6	37	27.5	7.1
1	7.5	4.1	405	+	1.75	3.76		7,7	250	633	\ <del>\</del>
e	12,0	4.5	4/0	+	1,40	2,27		36	2 5	27.2.	11/4
7	150	4.5	410	_	1,25			96	8	hss	7.3
8	121	7.7	014		7. 20	ا ـ ا		36	1,6	254	44
8	200	7.7	409	7	1.20	3.12		99	16	253	24
0)	22.5		20%	+	,20	3.12		200	177	2 1.3	3.2
12,	27.6	4.5	297	+	22	3.47		7,0	1/2	7.57	7/4
	17	(025)	, ,		<b>/</b>	7 7 6	47.942		,		7
				-			•				
		Tm = 41		-					1		
		()	393		77	137	£ 2.38	20	16		
				+	177	1 July 2			•		
		- HS	3.07								
		1 4678	7.								
			21.5 (8/2	+				+			

4^

	AIR POLL	UTI	ON PARTICUI	LATE ANA	LYTICAL	LDATA		
BASE	C	ATE	2 JUNE	89		RUN NUMBER		
EIEL SCAL				SOURCE NI	MAED			<del></del>
BLD6 6203	POWA	ER	PLITAT			2.#4		
1.			PARTICU	ILATES	<del>-</del>			
ITEM			FINAL W (gm)		INIT	IAL WEIGHT		VEIGHT PARTICLES
FILTER NUMBER	· · · · · · · · · · · · · · · · · · ·		0.55	87	<u> </u>	2874	(	0,2713
ACETONE WASHINGS (Prob Hall Filter)	e, Front		98.80	181	1 <del>02</del>	· 6686 -7352	0	. 2293
BACK HALF (II needed)								
			Total We	ight of Partic	culates Coll	ecred	C	0,5006 am
11.			WAT	ER				
ITEM	<del></del>		FINAL WE		INIT	IAL WEIGHT (gm)		WEIGHT WATER (@m)
IMPINGER † (H20)			144	/	10	00		44
IMPINGER 2 (H20)			142		10	00		42
IMPINGER 3 (Dry)			10.6			0		10.6
IMPINGER 4 (SIIIca Gel)	IMPINGER 4 (SIIIca Gel)			1	2	00		25.1
			Total Wei	ight of Water	Collected		/	22 gm
101.			GASES			r		
ITEM	ANALYSIS 1		ANALYSIS		LYSIS ANALYSIS			AVERAGE
VOL % CO2	10.4		10.6	10.	6			10.5
VOL → 0 <sub>2</sub>	8.3		8.3	8.	2			10.5
VOL % CO								
VOL % N2								
		Vol %	N <sub>2</sub> = (100% - % (	02.%02.	% CO)			

RUN HUMBER  # 2  DATE    2	SCHE	SCHEMATIC OF STACK CROSS SECTION	SECTION	EQUATIONS			AMBIE	AMBIENT TEMP	
				•				70	о 40
		Ü	the state of the s	OR = OF + 460			STATI		
	7		Perx	H = 5130.	5130.Fd.Cp.A 2	Tm. Vp	1	29.2	In Hg
<del>1</del>	273	4678		`	າ ູ້	S		250	qo Ч
				prelia	preliak-ducko (5" 4g-1000	12 Mg-1		PROBE HEATER SETTING $250$	<u>ن</u>
METER BOX HUMBER  # 2  Qw/Qm  TRAVERSE SAMPLIN POINT TIME NUMBER (min)  2 2 2 7 3 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4 4	<i>,</i>			المجازات	pick-to be chel	el - 900	1	PROBE LENGTH	
Co TRAVERSE SAMPLIN POINT TIME NUMBER (min)		C XX		i ext	iah Shel	-good	NOZZI	NOZZLE AREA (A) - DIA	
TRAVERSE SAMPLIN FOUNT TIME NUMBER (ain)	<del></del>	No of the state of			, Cab 10 "H2"	_	ථ	44	4.03
TRAVERSE SAMPLIN POINT TIME NUMBER (BIN)	\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\\	7		Scoj	Soot Brow	30	DRY G	DRY GAS FRACTION (Fd)	ਰ
NUMBER (BIN)  2 2.7  3 4 6  4 4.7	6 Weigh	. STACK TE	VELOCITY	ORIFICE	GAS	AS M	7 <b>#</b>	3 SAMPLE	I IMPINGER
7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7 7	THE HOUSE	(OF) (Ts) (OR)	HEAD (Vp)	PRESS.	VOLUME (cu ft)	N (9)	AVG 0UT (Tm) (oF)	TEMP (OF)	TEMP (OF)
2.7.	3.5	7,00	1.07	2.14	82,537	33		240	8
3 7 9 3	6.9	Aoa	1.40	3.64		8 8	8.8	146	6.3
	2,5	404	37	3,76		25	ž &	241	43
	7 4	717	5h.)	3.73		76	8	HHE	83
	5,0	4/12	1,46	3.61		36	87	242	13
	7,7	412	1.30	3.3%		7.5	5	246	9,5
3 (7.5)	2,3	2) 6	1.25	5.23			2,0	348	00/
2 2	ع ز	217	1.20	3. (1		100	2 2	0 47	50%
	4.0	714	(.20	3.12		101	4.3	253	1,01
12	M	411	86,	3.55		101	47	122	103
3000	130				117,93				
						-			

\ 51

THE STAND ST					ARTICULATE	SAMPLING DATA	SHEET				
### 2 2/2    1	RUN NUMBER		SCHEMA	TIC OF STACK CR	OSS SECTION	EQUATIONS			AMBIEN	r TEMP	
1	#2	7	7			OR = OF + 46	٥				9 P
### The continues in the continues of th	1					_	2		0   \   \   \   \	PRESS	i Ho
THE BOX NUMBER  SOME THAT IN THE STANDARD CONTROL OF FIGURE CHARTER SETTING  THAVERSE SAMPLING  SOME THAVERSE  SOME THAVE SAMPLE  SOME THAVENOUS TO SOME THAVE SAMPLE  SOME THAVE THAVE SAMPLE  SOME THAVENOUS TO SOME THAVE SAMPLE  SOME THAVE THAVE SAMPLE  SOME THAVE SAMPLE  SOME THAVE AND THAVE SAMPLE  SOME THAVE SAMPLE  SOME THAVE AND THAVE SAMPLE  SOME THAVE SAMPLE  SOME THAVE AND THAVE SAMPLE  SOME THAVE AND THAVE SAMPLE  SOME THAVENOUS TO SOME THAVE SAMPLE  SOME THAVE SAMPLE  SOME THAVE AND THAVE SAMPLE  SOME THAVE SAMPLE	)	1				•			HEATER	BOX TEMP	c .
Column   C	BASE		1						PROBE	HEATER SETTIN	
Comparison   Com	SAMPLE BOX	KNUMBER							PROBE	ENGTH	
Co   Co   Co   Co   Co   Co   Co   Co											uı
Co	METER BOX	NO NO ER					•		NOZ ZLE		sa fr
Continue   1990   Continue   1990   Continue   Contin	Qw/Qm					<del> </del>			ථ		
TANVERSE SAMPLING  TANVERSE TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TANVERSE  TO STATE TO TEST TO THE TO	3		(A)						DRY GA	S FRACTION (FO	G
NOWER (ain) A (ALMS) (78) (78) (78) (78) (78) (78) (78) (78	TRAVERSE	-	SI <b>MI</b> S.	STACK TEMP	$\vdash$	ORIFICE	GAS	GASMETER	remp?	3 SAMPLE 4	IMPINGER
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		TIME (min)	CAL HADE			PRESS.			OUT (0F)	BOX TEMP	OUTLET TEMP (OF)
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	-			302	116.	3-78	-	+	43	273	176
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		2,7		700	1. (0			15	: I	787	2
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	2	2.2	0.7	700	1.30	3.41			00	7	778
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	*	1	2 4	102	-	15.5		7	1	- 11	6
7 $(5.5)$ $4.6$ $(130)$ $3.39$ $(10)$ $93$ $385$ $8$ $8$ $8$ $8$ $94$ $95$ $98$ $8$ $8$ $94$ $95$ $98$ $97$ $98$ $98$ $98$ $98$ $99$ $99$ $99$ $99$	~ ~	6.0	7.7 7.7	411	7	3.39	/	60	523	788	voa
3       4       3       3       3       4       3       3       3       4       3       3       3       4       3       3       4       3       3       4       3       3       4       3       3       3       4	1	15.0	4.5		087	3.38		اه ا	93	285	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	8	165	7.	+	1.30	3.38		37	65	288	
12 25.0 410 1.10 2.85 95 95 73 290 12 25.0 (770) 410 .69 1.80 140, 195 32. $\frac{1}{1}$	2 3	200	2 2 5 2	0/2	1.10	2,24		49	76	200	7 C X
72 22.5 (972) 41069 1.80 1.00 93 29(  30.0 (972) 1.80 1.40, 1995  1.80 1.40, 1995  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 39(  1.80 1.80 1.80 1.80 39(  1.80 1.80 1.80 1.80 39(  1.80 1.80 1.80 1.80 1.80 1.80 1.80 1.80	77	25.0		411	07.1	2.85	5	56	43	290	87
30.0 (770) 1/m = 44 1/s = 400.2 1/h = 3.22 1/h = 3.22 1/h = 3.22	11			01 h	69.	1,80	,	0.0	93	29(	88
1m = 44 TS = 400.2 MH = 3.22 BTS = 32.4204		0	(d)				+				
17 = 400.2 14 = 3.22 14 = 32.4204 15 = 400.2											
15 = 400.6 414 = 3.22 RTS = 32.420			7				51	6380	23		
BTS = 32,420			7 1	5.5							
		B	= 3%	420							
				_							

	AIR POLI	UTI	ON PARTICUI	ATE ANA	LYTICA	DATA		
BASE		ATE		- AIIA		RUN NUMBER		
EIELSON	,	, -	7 T :0//	T. 161	,	RUN#	7	
BUILDING NUMBER	-/	12	ZJUNK	SOURCE NU	MBER	KUN A		•
BLDG 6203	POWER	. 1-	TNFINE	13014	ER ;	#-4		
<u> -</u>			PARTIC					
	TEM		FINAL W		INIT	'IAL WEIGHT (gm)	<u> </u> '	VEIGHT PARTICLES (4m)
FILTER NUMBER			0.4	117	0.	2884	(	0.1833
ACETONE WASHINGS Hall Filter)	i (Probe, Front		102.8	578	102.	7352	0	0.1226
BACK HALF (If needs	od)	<b></b>						
			Total We	ight of Partic	ulates Coll	ected	0	, 3059 <sub>sm</sub>
11.			WAT	ER				
	TEM		FINAL WE		INIT	IAL WEIGHT		WEIGHT WATER
IMPINGER 1 (H20)			122	)		00		22
IMPINGER 2 (H20)		•	152			00		52
IMPINGER 3 (Dry)			26,	6		0		26.6
IMPINGER 4 (Silica Gel)			230.5		2	00		30,5
			Total We	ight of Water				131 am
10.			CASES	T				
ITEM	ANALYSIS		ANALYSIS 2	ANAL	YSIS 3	ANALYSIS		AVERAGE
VOL % CO <sub>2</sub>	10.6		10.6	10.	6			10.6
VOL % 0 <sub>2</sub>	8.2		8.4	8.	4			8.3
VOL % CO			*****					
VOL % N <sub>2</sub>								
		Vol %	N <sub>2</sub> = (100% - % (	02-%02-	K CO)			

					PART	PARTICULATE SA	SAMPLING DATA	SHEET					
•	ĮΦ	_		SCHEMATIC OF STACK CROSS SECTION	K CROSS'S	ECTION	EQUATIONS				AMBIEN	AMBIENT TENP	
	#3	1/2				,	0 = 0F + 460	ć				20	<u>د</u> د
	1	5				maker	- - - - -	Γ			STATIO	STATION PRESS	
	75-71	SUME ST				So 7€	H = 5130	5130.Fd.Cp.A 2	Tm Vp			29.20	De in Hg
	RWIER A.	RUKE ALYNT BUG 6203		Z &	B		.J	<b>-</b> 7 :	Ts.	•		HEATER BOX TEMP	90
	BASE	1 263		$\mathcal{C}$			Pie leuk Chi	Pre lough 660. 12 3 15 1/3 - 600 J	9 :	<i>≥</i> 3	PROBE	PROBE HEATER SETTING	9
	SAMPLE BOX NUMBER	UMBER	<u> </u> 				P. lot tube	Pilottube Check - Good	J. Car		PROBE	PROBE LENGTH	
			_		<b>د</b>		Post leak	Post 124/ clerk - @ 19 "H	J. 11 G			72	in
	METER BOX NUMBER	MBER		) To	_		-	•	600	•	NOZZL	NOZZLE AREA (A) D/)	t//
-	0w/Qm			177	1				<b>S</b>		ප	4	hi he
	3		1 3								DRY GA	ORY GAS FRACTION (Fd)	6
	TRAVERSE	SAMPLING	STATE	STACK TEMP	TEMP	VELOCITY	ORIFICE	GAS	GAS	GAS METER TEMP		SAMPLE	
٠٠٤/	NUMBER		PRESSURE (An H20)	l (oF)	(Ts) (oR)	HEAD (Vp)	PRESS.	SAMPLE VOLUME	(0 IN	AVG (Tmg)	700T	BOX TEMP	4 OUTLET TEMP
	,	Q		200		56.	3-20	148.33	18		87	228	10,
Ž.	R	2.5		400		1.20	3.12		90		30	242	79
	~	6.0		100		1,30	3.40		36		90	344	62
	ī	7.5		07/2		1.30	3.36		27		90	31,7	89
	7	200	77	417		2	336		36		30	27.7	7.5
		15.0	1	11/2		1,30	3 27		100		70	34.5	77
لي	O'4	17.5	13	II.		1,30	3.36		S.		3/5	1.13	700
	4	30.0	Ĭ	HIH		1.25	3.23		9.9		16	250	2
	0/	33.5	5,	414		1,20	3.11		00/		42	75-0	90
125	= ==	35.0	20	+ \( \frac{1}{2} \)		070	3.16		000		4	250	\$ 3
· · ·	1.0	30.0 (Stad)	7	1			7.50				77	757	
								171 500			+		
								2131					
				+									
								3			1		
لميا													
ل													
				+									
فيسند	1 1										+		
	DEHL FORM	. 18									1		

### STATION PRESS   1												
	RUN NUMBER	`	SCHEMA	TIC OF STAC	CK CROSS S	ECTION	EQUATIONS			AMB AMB		
	H	<b>\</b> '					$^{\circ}R = ^{\circ}F + 46$	0		STAT	ON PRESS	
##   Prof.   P	2	6231					_	2				
STATE FOR THURSER   STACK TEMP   STACK TEM	1						ų.			HEAT	ER BOX TEMP	
STATE BOX NUMBER   STATE   S	BASE						!	,		PROB	E HEATER SETT	S
Co	1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1	0 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1 1								PROB	E LENGTH	
Columbration   Colu												
Compared	METER BOX N	UMBER								NOZZ	AREA	
Traverse   Sampling   Stack temp   Velocity   Onifice   Gas Meter temp   Dev Gas Praction (FB)	Qw/Qm							•		ථ		
Thaveese sampling struck tend the position of	<b>3</b>									DRY	SAS FRACTION (F	9
Provided Statistics   Corp.			7 7 7		TEMP	7, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1, 1,	ORIFICE	GAS	GAS ME	TER TEMP	SAMPLE	1
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		SAMPLING TIME (min)	PAESSURE (in H20)	l (oF)	(Ts)	HEAD HEAD (VP)	DIFF.	SAMPLE VOLUME	-	-	S BOX TEMP	3 ·
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		1		1331		64.	24,4		+	<del>[</del>	2417	
$\frac{3}{1}$ $\frac{5}{1}$ $\frac{5}$	ĺ	35	0/	Coh		04.1	3.65		76	71	156	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$		5.0	17	100		1.50	2.93		16	14	251	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	17	25	18	7/17		04-1	5.63		37,	→ r	250	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	٠,	10.0	01	717		07/	3.6.3		900	450	157	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	۲ و	16.6	6/	77.17		27:	3.7 K		44	6	2//5	650
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	2	26/	15	1112		07.1	3./0		97		1,1	
$\begin{array}{c ccccccccccccccccccccccccccccccccccc$	6	20.02	15	711,		1	3. (0		36	7(	547	
$\begin{array}{cccccccccccccccccccccccccccccccccccc$	707	22.5	41	717		1.20	3.10		- 56		2.50	
3.5 (5to <sub>2</sub> )  3.5 (5to <sub>2</sub> )  7.5 (5to <sub>2</sub> )	Ţ	27.5	7.7	413		1,20	5.10		300	_ 1 -	351	
= 104 = 105,315 VOL = 56,9 = 200 = 10515 = 30,534	ړ	.17	10	(		73.17	* 10					
= 394								14 7/21		l l	0.50	
= 20 43 AH = 20 3.534 = 294 17515 = 31.534					1			10101	2	١	3	
= 394 p515=					1	AN 93	1		3.23	+		
394					11	TAXA	176	NACON SAN				
						39H		31.534				
												_

	AIR POL	LUTI	ON PARTICU	LATE ANA	LYTICA	L DATA		
BASE		DATE				RUN NUMBER		
EIELSON	<b>,</b>	1	2 JUNIE	59		#3		
BUILDING NUMBER				SOURCE NO	IMBER	<u> </u>		
	POWER PLA	~7	_	1301	LER	#4		
i			PARTIC	JLATES	· · · · · · · · · · · · · · · · · · ·		<del></del>	
	ITEM		FINAL W		INIT	TAL WEIGHT (gm)	'	VEIGHT PARTICLES (gm)
FILTER NUMBER			0.46	602	0.	2897		0.1705
ACETONE WASHING Hall Filter)	S (Probe, Front		93.7	880	93	.6284	6	0.1705
BACK HALF (II need	led)							
			Total We	ight of Partic	culates Coll	ected	0	7,3301 #
и.			WAT	ER				
	ITEM		FINAL WI		INIT	IAL WEIGHT		WEIGHT WATER
IMPINGER 1 (H20)			144	<i>(</i>	10	00		44
IMPINGER 2 (H20)			132		/ (	00		32
IMPINGER 3 (Dry)			10			0		10
IMPINGER 4 (Silica Gal)			225.1		2	00		25.1
				ight of Water				/// gm
III.	ANALYSIS		GASES	(Dry)	Y515	ANALYSIS		
ITEM	1		2		3	4		AVERAGE
VOL % CO <sub>2</sub>	10.8		11.0	//	.0			10.9
VOL % 0 <sub>2</sub>	8.2		8.2	8.	2			10.9
VOL % CO		<del></del>	·					
VOL % N <sub>2</sub>								
		Vol 7	i N <sub>2</sub> = (100% - % (	CO <sub>2</sub> - % O <sub>2</sub> .	% CO)			

AFOEHL

CERTIFIED DY

Sun Location Line

AUDITIONAL INFORMATION

No. 3

COMPANY MAJUE	0838	AVATION	DATE		START	TIME 1/2   END TIME
WSAT	12	Jun	ż 89		12	1323
STREET ADDRESS	SEC	0	15	30	45	COMMENTS
		5	5	5	5	
	b3	12		T		
EIR SON AFB STATE ZIP	2	5	5	5	5	
1 FRUNE RET CONTECTS 1 DOUNCE IS NOWGEN	3 25	15	12	10	10	
George Ponche Boiler # 4	4	5	5	5	5	
PROCESS EQUIPMENT OPERATING MODE	5	10	5	5	5	
Coaltred Borles 100 Klbs Ho/M CONTROL ECUIPMENT OPERATING MODE	6		5	5	5	
Cyclone separators nom.	7	5	5	5	.5	
DESCRIBE EMISSION POINT Steel Stack	8	5	5	5	5	
Steel Stack	9	10	5	5	5	
	10,	10	5.	10	5	,
HEIGHT ABOVE GROUND LEVEL HEIGHT RELATIVE TO OBSERVER  100 + Start 6 End	11	5	110	5	5	
DISTANCE FROM OBSERVER / DIRECTION FROM OBSERVER /	12	5	5	5	5	
Start SO End Start NNE End	13					
DESCRIBE EMISSIONS	14					
Stan Biogens End V EMISSION COLOR / IF WATER DROPLET PLUME	15					
Start White End Attached   11/17 Detached	16	-				
POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED  Start 0 - 5 work Stack End	17					
DESCRIBE PLUME BACKGROUND	18					
Sian Bla. Skur End L		<del> </del>				
BACKGROUND CCLOR / SKY CONDITIONS	19					
Start Blue End Start End  WIND SPEED WIND DIRECTION	20	-				
Start 45 End V Start VRB End	21		-			<u> </u>
AMBIENT TEMP   WET BULB TEMP   RH. percent   Start 73   End	22					
Stack SOURCE LAYOUT SKETCH Draw North Arrow	23					
Plume	24					
Sun 💠	25					
	26					
Emission Point	27				·	
	28					
/	29					
	30					
	OBSE	AYEA'S N	IAME (PF	TINE CINE	cott	-
Observer's Position	OBSE	rau RVFA's s			9011	DATE
140.		Pan	(7/	CIAF		12 June
Fun Location Line		NIZATION FUE	+1 /1	E( W	AL	Function
ADDITIONAL INFOCMATION	CERT	FIED BY			(ĵ	DATE M. 1 69
59	100	un Air	Luti	2/ 150	المماو	1 n M, , 8 49

APPENDIX F Boiler 4, Field Data, 14 July 89

		YEY DATA SHEET NO. 2 Cemperature Traverse)	
BOILER NUMBER		14 JUNE 89	
H 4 INSIDE STACK DIAMETER # 52 STATION PRESSURE			Inches
STACK STATIC PRESSURE			In Hg
SAMPLING TEAM  WFOEHL	,7a -		In H20
TRAVERSE POINT NUMBER	VELOCITY HEAD, Vp IN H20	√ V <sub>P</sub>	STACK TEMPERATURE (0F)
<b>/</b> .	, 91		392
. 2	1,3		393
3	1.3		395
4	1. 3		395
5	1. 2		395
6	1.10		394
7	.94		394
8	,90		393
9	. 86		393
16	,84		391
	.85		388
12	767,70		389
	+ //sec =	73	
	Ī; =	393	
	$\Delta P = 1$	,	
	Nuzzl	214 = 0.2381	
	actuu	1 Dia = 0 Z5	
	AVERAGE		

RUN NUMBER			TIC OF STA	SCHEMATIC OF STACK CROSS SECTION	ROSS SECTION EQUATIONS	EQUATIONS		0001	$\vdash$	AMBIENT TEMP	
#	) <u> </u>	7				$^{\circ}R = ^{\circ}F + 460$	0		ė	STATION OBJECT	90
PY JUNE 84	hs 3				- meter	5130	St.Co.A ] 2	Ta		38 96 g	in Hg
PLANT Day 6.0	D. 4.1. T				7	# #	°	Ts . vp	Ŧ	HEATER BOX TEMP	
BASE RIFICOL	614		S C	4	⋖	1 told 10	glot tube thock - goed	Brok		PROBE HEATER SETTING	TTING
SAMPLE BOX NUMBER	NUMBER		<i>\</i>	<u>`</u>		Pie lee	k check & "	5 "M3 - 5c	<del></del>	PROBE LENGTH	
METER BOX NUMBER	UMBER	<u> </u>		$\rangle  $		Post Le	Post Louk thock @ 13' Mg- 600d	- 64, E)	ــــــــــــــــــــــــــــــــــــــ	NOZZLE AREK (A) - DIF	
<b>Ç</b> w.∕ Øm Co			101	70/		5007	B106		<u>0</u> 5	CP . Y 4 DRY GAS FRACTION (FG)	
TOAVERCE	07	74.7	TAC	STACK TEMP	×1:00:197	ORIFICE	GAS	G GAS M	GAS METER TEMP 7	~	77
POINT POINT	TIME TIME	PRESSURE (In H20)	(0F)	(Ts) (°R)	HEAD (VP)	DIFF. PRESS. (H)	SAMPLE VOLUME (cu ft)	iN (OF)	AVG OUT (Tm) (0F)	<del> </del>	OUTLET TEMP (OF)
	0		333		1.1	3.62	306.500	67	$\vdash$		$\left  \cdot \right $
~	2 5		393		(3	2.86		7.9	65	360	53
~ :		4	388		4.3	213		63	66	3 7	53
	10		300		2	2,89		73	100	200	578
و	12.5	į	333		1.1	3,65		1.5	67	Н	64
7	15.5		344		66.	a.38		75	6	284	67
مح اعات	7.75	3.5	394		60	18.K		J-(E	7 3 3	1 00 m	7.
0,	3).5	3.5	3471		6	2.19		76	300	-	76
1 -	25	2.5	39.1		63,	27.12		75	69	082	75
71	1		394		١8,	60. ه		75	ο 2 2		72
2	30 (Stop						330,431				

UEML CHE 18

				PART	ICULATE SA	PARTICULATE SAMPLING DATA SHEET	SHEET					
S S S A S I S I S I S I S I S I S I S I		KENE	SCHEWATIC DE STAPE PORSE SECTION	יר הפתנני	PATION	BOLLA TIONS				AMBIEN	AMBIENT TEMP	
# 1	, c	,		ב בניסט	N .	S C C C C C C C C C C C C C C C C C C C						(
DATE	\i	1				$^{\circ}R = ^{\circ}F + 460$	0			STATIO	STATION PRESS	P
21 47 11	ני ציני						7 2	,		2	9.96.0	11 -11
1	100					Н # 5130		T v v		HEATER	HEATER BOX TEMP	au ur
						J	7	ı •				90
BASE										PROBE	PROBE HEATER SETTING	
SAMPLE BOX NUMBER	NUMBER	<b>—</b>								PROBE	PROBE LENGTH	
												. <u>\$</u>
METER BOX NUMBER	UMBER									NOZZLE	E AREA (A)	
Qw/Qm										ථ		sq ft
ပိ		-								DRY GA	DRY GAS FRACTION (Fd)	ଟ
TRAVERSE	SAMPLING	STATIC	STACK TEMP	TEMP	VELOCITY	ORIFICE	GAS	( GAS	GAS METER TE	TEMP 7	, SAMPLE	V IMPINGER
POINT	TIME (min)	PRESSURE (10-H20)	(0F)	(Ts) (°R)	HEAD (Vp)	DIFF. PRESS. (H)	SAMPLE VOLUME (cu ft)	IN (OF)	AVG (Tm) (Rg)	out (oF)	S BOX TEMP (PF)	OUTLET TEMP
3c 1	્		39.3		153	1.27	230.931	۲۲		89	८१६ म	63
7	2.5		393		١٠٠,	9 K. K		73		39	346	59
3	5.0	3.5	385		1.1	۵		75		63	341	00
-	7.5		393		- '-			76		69	344	00
	, o c	3.0	397			9.64		2,1		59	3 40	60
٦٤٠	(7)		278			- 6		- !		1,0	37.0	60
- 3	7.0		190			79.6		7.0	<u> </u>	2/0	320	53
,, e-	26	3.0	399		1 - 1	2,65		79		1,2	246	09
וק	23.5	1	399		7	1 .		73		71	141	60
-	2,2		398		66′			79		7.1	1	09
	2	0.0	39.7		06.	9.18		80		73	248	99
3	3 c (576)						255.025		THE STATE OF THE S			
			300		AN CHARLE	1 12/13/BI			2			
	j											
	/m :	7/			1	2	30.0		1			
	15 5	394			1214		101 VQ.	8h =	525	#3		
	5 11 3	2.51										
	- 2150	79.7271										
PER FORM											7	

OEHL FORM 18

65

	AIR POLL	UTION PARTICUL	ATE ANA	LYTICAL	DATA	
BASE	1	PATE	-		RUN NUMBER	
EIELSON		14 JUNE	89		#1	
BUILDING NUMBER			SOURCE NU		_	
BLDG- 6203	POWER 1	PLANT	B016	TER F	¥ 4	
1.		PARTICU		· · · · · · · · · · · · · · · · · · ·		
ITE	EM	FINAL WE		INIT	IAL WEIGHT	WEIGHT PARTICLES (@m)
FILTER NUMBER		0.45	39	0.	2843	0.1696
ACETONE WASHINGS (P Hall Filter)	Probe, Front	98.8	264	98.	6688	0.1576
BACK HALF (if needed)						
		Total We	ight of Partic	ulates Coll	ected	0.3272
н,		WATE	ER			
ITE	M	FINAL WE	IGHT	INIT	IAL WEIGHT (gm)	WEIGHT WATER (@m)
IMPINGER 4 (H20)		126	M/s	/	00	26 Ms
IMPINGER (H2U)		178	pals	/ 4	00	78 M.S
IMPINGER 3 (Dry)		6	6 m/s		0	6 M/s
IMPINGER 4 (Silica Gel)		219.	219.79		00	19.799
			Total Weight of Water			130 gm
III.  ITEM ANALYSIS 1		GASES ANALYSIS 2	ANAL	YSIS 3	ANALYSIS	AVERAGE
VOL % CO2	12.4	12.6				12.5
VOL 7 0 <sub>2</sub>	6.8	6.7	6	3 -		12.5 6. <b>8</b>
VOL % CO						
VOL % N2						
	,	Vol % N2 = (100% - % C	:02 - % 02 -	% CO)		

			PA	PARTICULATE SAMPLING DATA SHEET	MPLING DATA	SHEET					
RUN NUMBER	117		SCHEMATIC OF STACK CROSS SECTION	SS SECTION	EQUATIONS			AMBIENT TEMP	TEMP	i c	
DATE					"R = "F + 460			STATION PRESS	4 PRESS	5	
14 JUNE 89	k 899				H = 5130.	5130-Fd-Cp.A 2 T	Ta	80	8 96 6	in Hg	
PLANT Div. /E.	0 6 52 17		66 C	А	_			HEATER	HEATER BOX TEMP	Ş	
BASE	1201					3		PROBE	PROBE HEATER SETTING	oF G	<b>_</b>
RIFLSCH	SCH	-	)		P.to+ +-	Pitot tale energy about	700L				
SAMPLE BOX N	NUMBER				Pre leak	P., leak (D 15" 4 - 600 )	1600 P	PROBE LENGTH	E LENGTH		
METER BOX N	MRED		(		•	)			7/0/11/5 1051 11/0/1/	Ē	
Z	K				77 + 6	11 1 401 166	July 16 16 16 16 16 16 16 16 16 16 16 16 16		MATER (1897)	7.	
ტ_/ტ			Je Je		. 56 .		. 0	ය	775		<del></del>
<b>ග</b>								DRY GAS	DRY GAS FRACTION (Fd)		
TRAVERSE	SAMPLING	STATIC	STACK TEMP	VELOCITY	ORIFICE	GAS	GAS METERT	TEMP 7	SAMPLE	4 IMPINGER	<del>-</del>
•	TIME 72 (min)	PRESSURE (in H20)	(oF) (Ts) (oR)	HE AD (Vp)	DIFF. PRESS.	SAMPLE VOLUME	N AVG (Tm)	Ė		OUTLET TEMP	
	2		293	15.8	1.30	755.54	+-	10/	つめて	49	
_ 1	2.5		393	. 1/8	1.15		7,	70	233	09	
3	5		393	.99	3,36		7.3	70	448	9.5	
	7.5		388	,	2,67		75	70	253	63	
,	9.		75°	1	3.65			7,	346	58	
2	<u> </u>		23.0	1, 1	0.60		78	1	300	1 2	
29	,75		390		3,65		78	1/2	35.7	09	
5	20		$\dashv$	1.1	3.65		78	73	とうと	<i>د</i> ع	
0 /	225		3967				73	4	264	93	
٠, ٢	275		29.0	66,	52.0	•	XO X	47	757	50	<u>.</u>
77	3, (510)	Ca			6,0	274,691		5	s		<del>, ,</del>
	[m =	75				101 JOI	49,381				<del></del>
	15 =	396									
	. 711/	7 50									
		4.50									<b>_</b> _
	PS15 =	29.6210									, ,
OEHL FORM	78 18						<b>T</b>				<b>→</b> (

HUN NUMBER  H 2-  DATE  IL JUN F 37  PLANT  BASE  SAMPLE BOX NUMBER  QW/QM  Co  TRAVERSE SAMPLING  Co  Co  TRAVERSE SAMPLING  TRAVERSE SAMPLING  TAVERSE  SAMPLING  Co  TRAVERSE  SAMPLING  Co  TRAVERSE  SAMPLING  TIME  1.3  1.3  2.5  2.5  2.5  2.5  2.5  2.5  3.5  5.5  8.5  8.5  8.5  8.5  8.5  8	7/2	SCHEMAT	SCHEMATIC OF STACK CROSS SECTION	A Table SEX	IAN	21.0.2.			TAMBI	AMBIENT TEMP	
DATE  ILL JUNE PLANT BASE  SAMPLE BOX NUMB METER BOX NUMB  CO  CO  CO  TRAVERSE POINT AC NUMBER	7			XC33 3EC1	<u>-</u>	EQUATIONS					
DATE    U JCN F.   PLANT   BASE  SAMPLE BOX NUMB  METER BOX NUMB  TRAVERSE  TO NUMBER  T						OR = OF + 460	0		1	STATION DEFEC	40 40
BASE  BASE  SAMPLE BOX NUMB  METER BOX NUMB  Co  Co  TRAVERSE  TRA						_	2			396.86	in He
SAMPLE BOX NUMB METER BOX NUMB QW/Qm TRAVERSE TOONT AC NUMBER AC N						H H	Co	Ts. Vp	HEAT	HEATER BOX TEMP	
METER BOX NUMB  QW/QM  TRAVERSE  TRAVERSE  POINT  AC NUMBER  AC NUMBER									PROB	PROBE HEATER SETTING	NG OF
Ow/Om TRAVERSE POINT A NUMBER  1									PROB	PROBE LENGTH	
CO TRAVERSE POINT A NUMBER  1									NOZZ	NOZZLE AREA (A)	qi
TRAVERSE POINT A PUMBER A									ථ		sq ft
TRAVERSE POINT A NUMBER									DRY	DRY GAS FRACTION (Fd)	િ
AC NUMBER A	-		STACK TEMP	-	FLOCITY	ORIFICE	GAS	GAS METER	ETER TEMP	SAMPLE	IMPINGER
- 41		PRESSURE		(Ts)	HEAD (Vp)	DIFF. PRESS. (H)	SAMPLE VOLUME (cu ft)	N (OF)	AVG OUT (Tm)	BOX TEMP	OUTLET TEMP (PF)
2			393		1.1	2.66	277.671	76	Н	267	97
	5		393		1.2	3.31		7.7	78	263	65
	_		393	+	7,	3.16		1	101	72.	99
	,	4	376	+	200	5. (7		177	1,4	456	30/
7) 7	5	K	396		٩	٠, ١		134	1,5		70
			398		1.			79	73	132	92
 .>-	5'		318		0.	111.6		20	13	259	80
	3	4	33.00	1	96,			9/2	75	306	ر الا
	33.5		3.40	+	, to				21.	465	700
71 Spr	37.5		290	-	300	ر در در		83	74	363	58
	(69/5) 1		3				304.975				
	-										
	-										

OEHL FORM 18

	AIR POLI	LUTI	ON PARTICU	LATE ANA	LYTICAL	L DATA			
BASE		DATE				RUN NUMBER		······································	
RIELSON		16	1 JUNE 8	39		#2			
BUILDING NUMBER	. <del></del>			SOURCE NU					
BLDG 620	3, POWE	2 <i>f</i>	LANT	BOILER	(#	4			
I.			PARTIC	JLATES					
1	TEM		FINAL W		INIT	IAL WEIGHT	•	EIGHT PARTICLES	
FILTER NUMBER			0.46	52	0.	2915	(	0.1737	
ACETONE WASHINGS Hall Filter)	(Probe, Front		102.8	8113	102	., 7352	(	0.076/	
BACK HALF (II neede	d)								
				ight of Partic	ulates Coll	ected	(	7,2498	
11.			WAT				1		
	rem		FINAL WE		TINI	IAL WEIGHT		WEIGHT WATER	
IMPINGER 1 (H20)			14	6	10	00		46	
IMPINGER 2 (H20)			14	0	10	20	1	40	
IMPINGER 3 (Dry)	IMPINGER 3 (Dry)			1.8	_	0	/	1.8	
IMPINGER 4 (Silica Ge	D		22	l D	2	00		20	
			Total We	ight of Water	Collected		118 em		
111.	ANALYSIS		GASES		Vere				
ITEM	ANALYSIS		ANALYSIS 2	ANAL	YS15 3	ANALYSIS		AVERAGE	
VOL % CO <sub>2</sub>	10.0		0.0	10	.0	10.0		10.0	
VOL % 02	9.2		9.4	9.6		9.2	_	1.2	
VOL % CO	/		,						
VOL % N2									
		Vol %	N <sub>2</sub> = (100% - % (	CO <sub>2</sub> - % O <sub>2</sub> -	% CO)				

	구0	in Hg		ING OF		ni	77		Fd)	IMPINGER	OUTLET TEMP	63	5.5	93	8-4	56	200	1 / S	~	62	62	9	-				
AMBIENT TEMP		STATION PRESS	HEATER BOX TEMP	PROBE HEATER SETTING		72	NOZZLE ABEA (A) A.A	h8'	DRY GAS FRACTION (Fd)	SAMPLE	BOX TEMP	233	243	249	450	351	37.10	252	253	A52	95A	247					
AMBIE		STATE CX	HEAT	PROB	_			ප	DRY	TER TEMP	AVG OUT (Tm) (OF)	-	70	20	0/	2/2	9	69	69	69	<b>6</b> 0	69	*				
		T E	T. vo	J 00 5	( D15"Hz		2017			GAS METER	N (F)	-	73	7.2	14	1,5	1/2/2	777	74	HL.	73	-	+		-		
SHEET		Fd-Co.A ] 2	°	i	eu K cheu		ر داد د الر (٥			GAS	SAMPLE VOLUME (cu ft)	305,669										}	330.014				
SAMPLING DATA	OR = OF + 460	5130	S	Ptot Check	pre tost leak check D15" Hy Loud		post leuk theck (212 19 good			ORIFICE	DIFF.	3.35	3.13	7	3.13	3,2	22.6	77.10	1	L 🔻	- 1	`	KLYST BIL	16.00			
		-7 meter	7							VELOCITY	HEAD (Vp)	36,	1.3	57	5.	6-		200	76.	۳۶.	06'	176					
PARTICULA SCHEMATIC OF STACK CROSS SECTION		1_	∫ *€	; }-	)		(	70	]	STACK TEMP	(Ts) (°R)	2	3		2				7		- 0	30					
MATIC OF			72	, <b>~</b>				111	7			33.	34	336	346	407	2 5	393	333	377	398	398			-		
SCHE										VATANC	PRESSURE Kn H20)	<b>∂</b> ≂			1	20			1		9						
	7/1	6.8	Like	יאנרא	SOM		MBER			SAMPLING	TIME A (min)	0	ک تو	5,	7.5	70		175	20	325	3.5	315	30(510p				
N NUMBER	#3	DATE 14 JUNE 89	PLANT	POWEY HIJAN	RIFICSON SAMPLE BOX NUMBER	#	METER BOX NUMBER	I	Co	TRAVERSE	POINT	- 21	۲	3	-	Λ	3	3	6	01	11	7,					

RUN NUMBER												
#3		SCHEMA	SCHEMATIC OF STACK CROS	K CROSS S	S SECTION	EQUATIONS				AMBIENT TEMP	LYEMP	
1	zh					00 = 0F + 460	c					<b>4</b> 0
- K						-	,			STATION PRESS	PRESS	
アン	JUNE 89					н 5130	5130-Fd-Cp-A 2	Tm		K	8.408	in Hg
PLANT	PLANT					 				HEATER	HEATER BOX TEMP	
MOD	また とうとび											ФF
BASE	/403	<del></del>								PROBE	PROBE HEATER SETTING	ی
こんじんご	777									110000		
SAMPLE BUX										TAGORY /	Lengin 72	
METER BOX NUMBER	IUMBER	1								NOZZLE	NOZZLE AREA-(A) DIA	
#2												***
₩/Qm										ථ	hs'	
ပိ		\ 								DRY GA	DRY GAS FRACTION (Fd)	
TRAVERSE	$\vdash$	STATIC	STACK TEMP	TEMP	VELOCITY	ORIFICE	GAS	GAS	GAS METER TEMP	d Ap	SAMPLE	IMPINGER
POINT NUMBER	TIME B (min)	PRESSURE	(0F)	(Ts) (°R)	HEAD (Vp)	PRESS.	SAMPLE VOLUME (Cu ff)	N (P)	A (Tage)	OUT (OF)	BOX TEMP (0F)	OUTLET TEMP (OF)
_	d		333		41.	1,77	330,214	17		1/3	346	35
ų	2.5		393		79.	2,33		73	)	(7	250	53
3	,5	و	387		1.0	4.42		73			348	53
4	75		396		1	2,63		73	7	57	250	<b>8</b> 3
Š	io		398		<b>か</b> て.	a.36		7,7	)	67	251	53
ور	12.5		400		1.0	3.38		73		oc e	352	53
7	15		399		0.1	3.38		73	)	67	348	53
<b>3</b> 7)	17.5		399		1.1	89.B		73		67	351	5
٠	2.0		700		1,1	2.63		74	9	800	254	24
)(	33.5		0.07		0.0	3.38		74		اح	355	54
=	25		399		16'	31.8		76	7	39	243	55
7 7	27.5		378		09	7.42		76		n	35	55
,	1	1,1					35 3.60 g		-	$\uparrow$		
	Th =	77.								(		
		7 20 0					10 L VOL	16	170 3	73		
	1/5 = 4	371								+		
	2 = 717	2,41										
	C = 7120	1990 pc										
		1 2 - 1 2							$\uparrow$			

OEHL FORM 18

	AIR POL	LUTI	ON PARTICU	LATE ANA	LYTICAL	L DATA		
BASE		DATE				RUN NUMBER		
FIELSON		/	4 JUNE	89		#3		
BUILDING NUMBER	<del></del>		<del></del>	SOURCE NU	MBER			
3406 620	3, POWER	PL	BUT	BOIL	FCR #	14		
1.			PARTIC	ULATES	· · · · · · · · · · · · · · · · · · ·			
	ITEM		FINAL W		INIT	IAL WEIGHT	*	EIGHT PARTICLES (gm)
FILTER NUMBER			0.47	73	0,.	2867	0	0.1906
ACETONE WASHING Hall Filter)	iS (Probe, Front		93.7.	152	93	6285	0	,0867
BACK HALF (il need	ded)							
			Total We	ight of Partic	ulates Coll	ecte !	0	,2773 m
II.			WAT					
·	ITEM		FINAL W		INIT	IAL WEIGHT (gm)		WEIGHT WATER
IMPINGER 1 (H20)			18	3	/	00		83.0
IMPINGER 2 (H20)			1/1	5	/	00		16,0
IMPINGER 3 (Dry)	IMPINGER 3 (Dry)			0.0		0		3.0
IMPINGER 4 (Silica C	Gel)		218.4			.00		18.4
			Total We	ight of Water	Collected		120	
111.		Γ—	GASES	T		T		
JTEM	ANALYSIS 1		ANALYSIS 2	ANAL	. YSIS 3	ANALYSIS 4		AVERAGE
VOL % CO2	10.4		10.6	/	0.6			16.5
VOL % 02	8.8		9.0	8	8			8.9
VOL % CO								
VOL % N2								
		Vol %	N <sub>2</sub> = (100% - %	CO <sub>2</sub> .%O <sub>2</sub> .	% CO)	·		

VISIBLE EMISSION OBSERVATION FORM

No. Me OBSERVATION DATE START TIME COMPANY NAME END TIME 8 102411) USATE STREET ADDRESS, 45 COMMENTS 15 30 STATE ZIP 3 PHONE (KEY CONTACT) Boile # 4 OPERATING MODE iooklbs ste 10 OPERATING MODE CONTROL EQUIPMENT 8 DESCRIBE EMISSION POINT 10 HEIGHT RELATIVE TO OBSERVER HEIGHT ABOVE GROUND LEVEL 100 + End / DISTANCE FROM OBSERVER DIRECTION FROM OBSERVER 12 End V 13 DESCRIBE EMISSIONS
Start Windows 14 EMISSION COLOR SIAN WITH THUMEND IF WATER DROPLET PLUME 15 Attached D | 1/1 Detached G 16 POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED 17 DESCRIBE PLUME BACKGROUND 18 <ky 19 Start Will En SKY CONDITIONS Start-OVC 20 WIND DIRECTION YAND SPEED Sian NE 21 Start 15 mg AMBIENT TEMP WET BULB TEMP RH, percent 22 66 <10 Start End 23 SOURCE LAYOUT SKETCH Draw North Arrow 24 Ш תורע Plume 25 Sun Wind 26 27 **Emission Poir** 28 29 OBSERVER'S NAME (PRINT) Observer's Position DATE JIM OBSERVER'S SIGNATURE ORGANIZATION Sun Location CERTIFIED BY ADDITIONAL INFORMATION 73

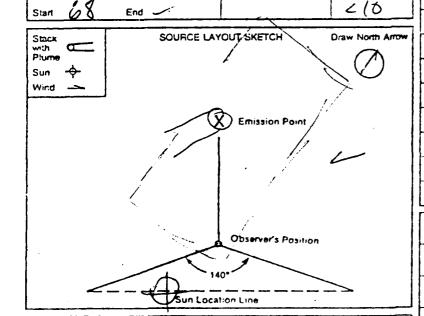
COMPANY NAME			Oase	AVATION	DATE	Tue	START	TIME 156	END TIME
STREET ADDRESS PP			SEC	0	15	30	45		COMMENTS
			1	5	5	5	5		
CITY / 11 ATO	STATE	ZIP	2	5	5	5	5		
1 Riplsm HH12 1	HK		3	5	5	10	5		<del></del>
PHONE, KEY CONTACTY THE TIS YELL	SOURCE ID NUMBER	4	4	5	5	5	10		
PROCESS EQUIPMENT : Coal-Bula		ATING MODE	5	10	5	5	5		
CONTROL ECUIPMENT	IOU K	165 Stearly	.26 .	5	5	5	5		
CONTROL ECCUPMENT.		Lima	7	5	5	5	5		
DESCRIBE EMISSION POINT	···		8	5	5	5	10		
Stel Stack			9	5	5	5	5		
			10	10	10	5	5		,
1 /	HEIGHT RELATIVE T	O OBSERVER	11	5	5	10	5		·····
DISTANCE FROM OBSERVER	DIRECTION FROM O	BSERVER	12	<	5	10	10		
Start 50 End V	Start NNW	End V	13				1.5		
DESCRIBE EMISSIONS		·	14						
EMISSION COLOR	End /	PLUME	15						
SIAN PRODUCTION THE PLUME AT WHICH OPACIT	Attached   P	Detached 🗆	16						
	Y WAS DETERMINED End	•	17		<del> </del>				
DESCRIBE PLUME BACKGROUND			18						
Start SKY	End		-						
BACKGROUND COLORIA	SKY CONDITIONS SIZE THE BKA		19		<del> </del>		<b></b>		
WIND SPEED /	WIND DIRECTION	End	20						
Stare 25 WINERD		End	21						
AMBIENT TEMP Start D End	WET BULB TEMP	RH, percent	22						
	N. S. C.		23			 			
Stack SOURCE LAYO	DUTSKETCH	Draw North Arrow	24						
Sun +			25						
Wind -		> /	26						
$\sqrt{\alpha}$	Emission Point	/ /	27						
	A		28						
	. 0/	′	29						
	1	/	30						
	fy/			DVES:2:	1000		<u></u>	1 /	······································
	Observer's Position		UBDE	aven's r	MAME (PF	<b>5</b> 4	th-	Cant	
	S Position		OBSE	1/	SIGNATU	RE /	1/		DATE TO GE
140	,×/		ORGA	/ acc	<del></del>	100			14 July
Sur Locat:	on Line ·	_>		450	EH	1			
ADDITIONAL INFORMATION		74		FIED BY DX G.1	Air	alve	e B	Boul	17 Marks

VISIBLE EMISSION OBSERVATION FORM COMPANY NAME USA F OBSERVATION DATE START TIME STREET ADDRESS 45 PHONE (KEY CONTACT)

Ted Ti Sdall SOURCE ID NUMBER PROCESS EQUIPMENT OPERATING MODE oal Box 100K/hr stea CONTROL EQUIPMENT OPERATING MODE Nound 9 134 10 HEIGHT RELATIVE TO OBSERVER HEIGHT ABOVE GROUND LEVEL 100+ End / DISTANCE FROM OBSERVER DIRECTION FROM OBSERVER Ho12 Start 50' End / Stan NNW DESCRIBE EMISSIONS
Stan
EMISSION COLOR End IF WATER DROPLET PLUME 15 Sian Bray White End Detached G 16 POINT IN THE PLUME AT WHICH OPACITY WAS DETERMINED SIAN 0-5 WAY 5THE END DESCRIBE PLUME BACKGROUND 18 Start Start BACKGROUND COLOR-ID
Start End SKY CONDITIONS Stan -BKN

COMMENTS 22 23 25 26 27 28 29 30 OBSERVER'S NAME (PRINT) OBSERVER'S SIGNATURE DATE Jun 87 ORGANIZATION HECEHL

DATE



WIND SPEED

AMBIENT TEMP

Stan 25 Kts End

ADDITIONAL INFORMATION

WIND DIRECTION

SIAN NE

HH, percent

APPENDIX G Acetone Blank Results

# BLANK ANALYTICAL DATA FORM

Plant EIELSON AFB
Sample location BLANK
Relative humidity
Liquid level marked and container sealed
Density of acetone ( $\rho_a$ ) 0.78
Blank volume (V <sub>a</sub> ) /OO ml
Blank volume (V <sub>a</sub> ) /00 ml  Date and time of wt /2 JUNE 1800 Gross wt 105.2623 mg
Date and time of wt 13 June 1800 Gross wt 105,2623 mg
Average gross wt 105, 2623 mg
Tare wt 105. 2623 mg
Weight of blank (m <sub>ab</sub> ) mg
$c_a = \frac{m_{ab}}{v_a \rho_a} = \frac{(0.0000)}{(100)(0.78)} = \frac{0.0000  \text{mg/g}}{}$
Note: In no case should a blank residue greater than 0.01 mg/g (or 0.001% of the blank weight) be subtracted from the sample weight.
Filter number
Filters Filter number mg
Date and time of wt mg
Date and time of wt Gross wt mg  Date and time of wt Gross wt mg
Date and time of wt Gross wt mg  Date and time of wt Gross wt mg  Average gross wt mg
Date and time of wt Gross wt mg  Date and time of wt Gross wt mg  Average gross wt mg  Tare wt mg
Date and time of wt Gross wt mg  Date and time of wt Gross wt mg  Average gross wt mg  Tare wt mg  Difference wt mg  Note: Average difference must be less than ±5 mg or 2% of total
Date and time of wt Gross wt mg  Date and time of wt Gross wt mg  Average gross wt mg  Tare wt mg  Difference wt mg  Note: Average difference must be less than ±5 mg or 2% of total sample weight whichever is greater.
Date and time of wt Gross wt mg  Date and time of wt Gross wt mg  Average gross wt mg  Tare wt mg  Difference wt mg  Note: Average difference must be less than ±5 mg or 2% of total sample weight whichever is greater.

Quality Assurance Handbook M5-5.4

APPENDIX H Emissions Calculations

XRON "NET	ru 51	XROM THE	TH 5.	XR0# -#8	THE F
RUN NUMBER		RUN NUMBER	;	RUN NUMBER	-
BOILER 4, RUN 1		BOILER 4, RUN 2	į	BOILER 4, RUN ?	
	RUM	DOILER IN NO. 4	RUN		P(Iz.
METER BOX Y?		METER BOX YO		METER BOX Y?	
1.0020	RUN	1.0020	RUK	1.0020	Pto.
DELTA H?		DELTA H?	,	DELTA H?	
3.0700	RUN	3.2200	RUN	3,2300	P(0.
BAR PRESS ?		BAR PRESS ?		BAR PRESS ?	•
29.2500	PUB	29,2500	RUN	29,2500	10(1)
METER VOL ?		METER VOL ?		METER VOL ?	•
55.3950	BÜR	57.6389	RUH:	56 <b>.90</b> 30	P10:
MTR TEMP F?		MTR TENP F?	1,	MTR TEMP F3	
91.0000	RUN	94.0000	RUH	93,0000	PUR
% OTHER GAS		% OTHER GAS		% OTHER GRS	•
REMOVED BEFORE		REMOVED BEFORE		REMOVED BEFORE	
DRY GAS METER ?		DRY GAS METER ?		DRY GAS METER ?	
	RUN	PAT GAO HETEK	RUN	pict and there.	Pijk.
STATIC HOH IN ?		STATIC HOH IN ?		STATIC HOH IH 2	-
-1.3000	RUN	-1,3000	RUN	-1.3000	RUN
STACK TEMP.		STACK TEMP.		STACK TEMP.	
393.0000	RUH	499,9999	RUN	394,0006	PUN
ML. WATER ?		ML. WATER ?		ML. WATER ?	
122.0000	RUK	131.0000	RUN	110.0000	pen:
IMP. % HOH = 9.9					•
IMP. 4 NUM - 242		IMP. % HOH = 10.2		IMP. % HOH = 8.8	
% HOH=9.9				* unu=1 6	
		% HOH=10.2		% HOH=8.8	
% CO2?		% CO2?		% CO2?	
10.5000	PUN .	10.6996	RUN	10,9000	Mük
% OXYGEH?		% OXYGEN?	P.V.	% OXYGEN?	
8.3000	RUN	8.389P	RUN	8.2000	Billy
% CO ?		% CO ?	17011	% CO ?	
	RUN	% CO :	RUN		ÞΩ.
MOL WT OTHER?	8.111	MOL WY OTHER?	DATE.	MOL WT OTHER?	
	RUK	HOL W. OTHER.	RUN		b(lir
MICH -20 04			•••	W: ( 2. 62	
MWd =30.01		NWd =30.03		MWd =30.87	
MW WET=28.83		MW WET=28.80		MW WET=29.01	
		110, 112, 42,114			
SORT PSTS 2				OODT DOTO O	
31.5287	PUN	SORT PSTS ?		SQRT PSTS 2 31.5314	pos.
TIME MIN ?	* C14	33.42 <del>8</del> 4	PUN	TIME MIN 7	F
60.0000	RUK	TIME MIN ?		68.0000	Pije.
HOZZLE DIA ?	NOP	60.0000	RUN	NOZZLE DIA ?	F 4
.2500	RUN	NOZZLE DIP 2			<b>5</b> (1)
STK DIA INCH ?		.2500	RUN	.2500 STK DIA INCH ?	F ."
52.0009	PUK	STK DIA INCH ?		52,0000	PH
<i>56.000.</i>		52. <b>00</b> 00	RUN	22,0075	* 0
* VOL MTR STP = 52.3	र्वद			* VOL MTP STD = 53.	ដូច្នា
STK PRES ABS = 29.		* YOL MTR STD = 54.	245	STK PRES ABS = 29	
YOU HOH GAS = 5.74		STK PRES ABS = 29	. 15	YOU HOW GAS = 5.1	
% MOISTURE = 9.88		VOL HOR GRS = 6.1		1. MOISTURE = 3.80	
MOL DRY GAS = 0.98	11	% MOISTURE = 10.2	1	MOL DRY GAS = 0.9	
% NITROGEN = 81.20		MOL DRY GAS = 0.8	96	% NITROGEK = 80.9	
MOL WT DRY = 30.0:		2 NITROGEN = 81.1		MOL WT DRY = 38.6	
MOL WT WET = 28.83		MOL WY DRY = 30.0	?	MOL WY WET = 29.0	
VELOCITY FPE = 78.		MOL WT WET = 28.8	ę.	VELOSITY FRS = 27	
STACK AREA = 14.75		VELOCITY FPS = 80		STACK AREA = 14.7	
STACK ACEM = 63 11		STACK AREA = 14.7	<u>.</u>	STACK ACEM = 68.8	
* STACK DOCEM = 37 5	i67.	STACK ACEM = 71.0		* STACK ESCEN = 77	e :
% ISOMINETIC = 10		* STACH DOOFM = 38	192.	1 ISOFINETIC = 1	
	•	: ISOMINETIC = 1	<b>92.4</b> 9	4 100 106 1. 1 1	

## XROM THRESELOT

RUN

RUN NUMBER BOILER 4, RUN 1, 12 JUNE RUN

VOL MTR STD ? 52.3990 STACK DSCFM 2

37,567.0000  $\mathsf{P} \mathsf{U}_{\mathsf{H}}$ FRONT 1/2 MG ?

500,6000

RUN BACK 1/2 MG ?

0.0000 PUN

F GR/DSCF = 0.1474

F MG/MMH = 337.3764

F LB/HP = 47,4736

F KG/HR = 21.5340

#### XROM \*MASSFLO\*

RUN NUMBER

BOILER 4, RUN 2, 12 JUNE

YOL MTR STD ?

54.2460 RUN

STACK DSCFM ?

38,192,0000 PUN

FRONT 1/2 MG ?

305.9000 RUK

BACK 1/2 MG ?

0.0000 RUN

F GR/DSCF = 0.0870

F MG/MMM = 199.1401

F LB/HR = 28.4888

F KG/HR = 12.9222

## XRON "MASSFLO"

RUN NUMBER

BOILER 4, RUN 3, 13 JUNE

VOL MTR STD ?

53.6520 PHN

STACK DECEM ?

37-854.0000

FRONT 1/2 MG ?

330.1000 PUN

BACK 1/2 MG 2

0.0000 Plik

F GR/DSCF = 0.0949

F MG/MMM = 217.2734

F LB/HF = 30.8079

F KG/HP = 13,9741

XROM "METH 5"	XROM THETH 5"	
RUN HUMBER	RUN NUMBER	XROK THETH 5"
BOILER 4, RUN 1, 14 JUNE	BOILER 4, RUN 2, 14 JUNE	RUN HUMBER
RUN	Kilin	BOILER 4, RUN 3, 14 JUNE
METER BOX Y?	METER BOX Y?	PUT METER DOU NO
1.0020 RUK	1.8020 RUN	METER BOX Y?
DELTA H?	DELTA H?	1.0020 RUN
2.5100 RUN	2.5000 RUN	DELTA H?
BAR PRESS ?	BAR PRESS ?	2.4100 RUN BAR PRESS 2
28.9680 RUM	28.9680 RUN	28,9680 PUN
METER VOL ?	METER VOL ?	METER VOL ?
48.5250 RUN	49.3810 RUN	47.9400 PUN
MTR TEMP F?	MTR TEMP F?	MTR TEMP F?
71.0000 RUN	75.0000 RUN	71.0000 PUK
% OTHER GAS	% OTHER GAS	% OTHER GAS
REMOVED BEFORE	REMOVED BEFORE	REMOVED BEFORE
DRY GAS METER ?	DRY GRS METER ?	DRY GAS METER ?
	PÚK	PUK
STATIC HOW IN ? 7200 RUN	STATIC HOH IN ? 7200 RUN	STATIC HOW IN ?
	*****	7200 RUK
STACK TEMP. 394.0000 RUN	STACK TEMP. 396.0000 RUN	STACK TEMP.
ML. WATER ?	ML. WATER ?	397.0000 RUH
130,0000 RUN	118.0000 RUN	ML. WATER ?
•••••	IMP. % HOH = 10.5	120.0000 RUN
IMP. % HOH = 11.5	1111 . 7. HON - 10.3	IMP. % HOH = 10.8
% HOH=11.5	% HOH=10.5	% U0U~16 O
4 100 1110	V	% HOH≈10.8
	:	
% C02?	. % C02?	7 002?
12.5000 RUN	10.0000 RUN	10.5000 RUN
% OXYGEN?	% OXYGEN?	% OXYGEN?
6.7000 RUN	9.2000 RUN	8.8000 PUN
% CO ?	% CO ?	% CO ?
RUN	RUN	PUM
MOL WT OTHER?	MOL MT OTHER?	MOL WT OTHER?
RUK	RUN	PUK
MNd =30,27	MNd =29.97	MMd =30.03
MW WET≈28.86	MW WET=28.72	MW WET=28.73
SORT PSTS 7	SORT PSTS ?	00DT 50TT .
29.7371 RUN	29.6210 RUN	SQRT PSTS ?
TIME MIN ?	TIME MIN ?	29,2984 RUI
60.0000 RUN	60.0000 RUN	TIME MIN ?
NOZZLE DIP ?	HOZZLE DIA ?	<b>60.0000 PUN</b> HOZZLE DIA 2
.2500 RUN	,2500 RUN	.2500 PUL
STK DIA INCH ?	STK DIA INCH ?	STK DIA INCH ?
52.0000 RUN	52 <b>.000</b> 0 RUN	52.0000 PUK
		72.
* YOL MTR STD = 47.107	* VOL MTR STD = 47.578	* VOL MTP STD = 46,527
STK PRES ABS = 28.92	STK PRES ABS = 28.92	STK PRES PPS = 28,92
VOL HOH GRS = 6.12	VOL HOW GAS = 5.55	<b>VOL HOH GAS = 5.65</b>
% MOISTURE = 11.50	% MOISTURE = 10.45	% MOISTURE = 10.87
MOL DRY GAS = 0.885	MOL DRY GAS = 0.895	MOL DRY GAS = 0.892
% NITROGEN = 80.89	% NITROGEN = 80.80	% HITROGEN = 80.70
MOL HT DRY = 30.27	MOL WT DRY = 29.97 MOL WT WET = 28.72	MOL WT DRY = 38.03
MOL NT NET = 28.86	VELOCITY FPS = 73,82	MOL MT MET = 28.73
VELOCITY FPS = 73.93	STACK APEG = 14.75	VELOCITY FPS = 73,99
STACK AREA = 14,75 STACK ACEM = 65,416.	STACK ACEN = 65.320.	STACK AREA = 14,75
* STACK DSCFM = 80,416.	* STACK DSCFM = 34,867.	STACK ACF* = 64.577.
* STHUR DOURD = 34,093. % ISOMINETIC = 98,25	1 150k INETIC = 38.45	* STACK DSCFM = 34.287,
4 1900,180(10 ± 70,20	A ESSENTIAL TO TOP TO	% ISOKINETIC = 57.91

## XROM "MASSELO"

RUN NUMBER BOILER 4, RUN 1, 14 JUNE

VOL MTR STD ? 47.1876 RUS STACK DSCFM ? RUH 34,593.6000

FRONT 1/2 MG 2 RUN 327.2000

BACK 1/2 MG ?

0.0000

F GR/DSCF = 0.1072 F MG/MMH = 245.2871 F LB/HR = 31.7830

F KG/HR = 14.4167

RUN HUMBER

BOILER 4, RUN 2, 14 JUNE

YOU MIR SID ?

RUN 47.5780

STACK DSCFM ?

34,867.0000 RUE

FRONT 1/2 MG ?

249.8000 RUN

BACK 1/2 MG ?

RUN 0.0000

F GR/BSCF = 0.0810

F MG/MMM = 185.4100

F LB/HR = 24.2147

F KG/HR = 10.9838

XROM \*MASSFLO\*

RUN NUMBER

BOILER 4, RUN 3, 14 JUNE PUN

YOU MIR STD ?

46.5278 RUN

STACK DSCFM ?

34,287.0000

FRONT 1/2 MG ?

277.3000

Pibl

BACK 1/2 MG ?

6.6666 RUN

PUN

F GR/DSCF = 0.0926

F MG/MMK = 210.4797

F LB/HR = 27.0304

F KG/HF = 12.2610

APPENDIX I Calibration Data

## NOZZLE CALIBRATION DATA FORM

Date	<u> </u>	Calib	rated by _		
Nozzle identification number	mm (in.)	Nozzle Diam D <sub>2</sub> ,	eter <sup>a</sup> D <sub>3</sub> , mm (in.)	ΔD, b mm (in.)	D <sub>avg</sub>
12 JUNE 4 (VI	.250	,250	.250	0	,250
HJode 4 in	1250	.250	,250	0	.250
			•	·	

where:

Quality Assurance Handbook M5-2.6

aD<sub>1,2,3</sub> = three different nozzles diameters, mm (in.); each diameter must be within (0.025 mm) 0.001 in.

b  $\Delta D = \text{maximum difference between any two diameters, mm (in.),}$   $\Delta D \leq (0.10 \text{ mm}) 0.004 \text{ in.}$ 

 $D_{avg} = average of D_1, D_2, and D_3$ 

# METER BOX CALIBRATION DATA AND CALCULATION FORM

(English units)

Date 21 Nov 88

Meter box number Nutsh #2

Barometric pressure,  $P_b = 30.02$  in. Hg Calibrated by Scott & Vaughn

		Gas v	olume	T	emperati	ure				
/AC_	Orifice manometer setting	Wet test meter (V,),	Dry gas meter (V <sub>d</sub> ),	Wet test meter (tw),	Dry Inlet (t <sub>d.</sub> ),	<pre>gas met Outlet (t d ),</pre>		Time (Θ),	v ·	AU/A
	(ΔΗ), in H <sub>2</sub> O	ft <sup>3</sup>	ft <sup>3</sup>	•F	°F	°F	°F	min	Y	in. H <sub>2</sub> 0
4.0	0.5	5	5.657	75 535	7.7 8.2	75 77	537.75	12.40	¢.9926	1.73
4.0	1.0	5	5.031	76 536	89	77 80	t i	,	1.6634	1.87
4.0	1.5	10	10.101	17 537	90	84	547.75	15.35	1.0001	1.97
4.0	2.0	10	10.230	78 538	97	85 87	552.¢	B.45	<i>6.9</i> 981	2.00
4.0		10	10/170	538	100	87 89	554.75	18.92	1.0065	1.97
4-0	4.0	10	19/191	78 538	165	91	557.ø	9.35	1.0061	1.92
							-	Avg	1.402	1,91

		- <del> </del>	
ΔH, in. H <sub>2</sub> O	<u>ΔΗ</u> 13.6	$Y_i = \frac{V_w P_b(t_d + 460)}{V_d(P_b + \frac{\Delta H}{13.6}) (t_w + 460)}$	$\Delta H\theta_{i} = \frac{0.0317 \Delta H}{P_{b} (t_{d} + 460)} \left[ \frac{(t_{w} + 460) \theta}{V_{w}} \right]^{2}$
0.5	0.0368	(5)(3¢.¢2)(537.75) (5.¢57)(3¢.¢2)+452)(535)	$\frac{(631)(5)}{(3002)(537.75)} \left(\frac{(535)(12.4)}{(5)}\right)^{2}$
1.0	0.073 <b>7</b>	(5×30.02×542.5) (5,831)(30.02+15.1)(536)	(0317) (1.0) (536) (9.14) 2 (30.02) (547.5) (536) (9.14)
1.5	0.110	(10) (30 02) (542.75) (10.161) (30.02, 15) (537)	(0317)(1.5) (538)(538)) <sup>2</sup> 130 52)(547.75) [10
2.0	0.147	(10) (3c.02) (552) (10.13) (20.42 + 2.0 ) 538)	(6317)(2.0) (538)/13.45) <sup>2</sup>
3.0	0.221	(10) (31.02) (554.75) (10,17)(30.02 + 2) (536)	(0317\30) (538\10.92) 2 (3002) (554.75) [538\10.92] 2
4.0	0.294	(10.191)(30.02) (557)	(0317)(4.4) (538)(9.35) 2 (30.01)(537) (538)(9.35)

If there is only one thermometer on the dry gas meter, record the temperature under  $\mathbf{t_d}$ .

Quality Assurance Handbook M4-2.3A (front side)

POSTTEST DRY GAS METER CALIBRATION DATA FORM (English units)

Post (lear (Eielson)) Pretest Y 1002 Date 23 Jun 89 Meter box number Nutech 2 Dry gas meter number Barometric pressure, P. = 29.12.5 in. Hg Test number One

Y ,		$V_{\rm w} P_{\rm b} (t_{\rm d} + 460)$	V /P + AH \/t + 460	(a (b 13.6) (w)	16 (1145) (5. 12) 540	14 (194-153) 5/	10.347 (29.15. 15.6) 541	
		<b>;</b>	. ri		0.989	40 0,991	285.0	- A
	Vacuum setting, in. Hg					40	92,5555 84547.5 551.5 16.12 4.6 10.982	
		i	Time (A)	Bin,	15.67	(5.83	16.12	
	eter	Average	こ	o Tæri	97 550 85 545 547.5 15.67 4.0 0.989	550 15.83	5.1.55	
ure	Dry gas meter	Inlet Outlet Average	(t <sub>d,</sub> ), (t <sub>d,</sub> ),	. F	85 85 545	13 554 82 54 6	2.547.5	
emperature				oF.	41550	23.55H	95.55	
T	Wet test	meter	(t €)	e e	50 540	1 45 1	541	
	Dry gas	meter	(v <sub>d</sub> ),	ft³	10,2(2	10,223	77.7	
Gas volume	Wet test	meter	(\s^2)	ft.	10	10	10	
Orifice	Banometer	setting,	(AH),	1n. H <sub>2</sub> 0	7)	7.	7.1	

a If there is only one thermometer on the dry gas meter, record the temperature under  $\mathsf{t}_d$ 

 $V_{\omega}$  = Gas volume passing through the wet test meter, ft.

 $V_d = Gas$  volume passing through the dry gas meter, ft<sup>3</sup>.

 $t_{\rm w}$  = Temperature of the gas in the wet test meter,  $^{
m o}{
m F}.$ 

1,052 (-4-> 0.952

yt 0.050

= Temperature of the inlet gas of the dry gas meter, oF.

= Temperature of the outlet gas of the dry gas meter, of.

 $t_d$  = Average temperature of the gas in the dry gas meter, obtained by the average of  $t_d$ , and  $t_d$ , °F.

 $\Delta H = Pressure differential across orifice, in. <math>H_20$ .

 $\vec{r}_{i}$  = Ratio of accuracy of wet test meter the dry gas meter for each run.

= Average ratio of accuracy of wet test meter to dry gas meter for all three runs; tolerance = pretest  $Y \neq 0.05 Y$ .

 $P_b$  = Barometric pressure, in. Hg.

= Time of calibration run, min.

Quality Assurance Handbook M4-2.4A

STACK SENSOR CALIBRATION: 19-20 Oct 88

SENSOR #	REFERENCE TEMPERATURE (deg K) X axis	TEST TEMPERATURE (deg K) Y axis	
P1	273.30 371.90 447.00		Regression Output:  Constant -4.30 Std Err of Y Est 0.20 R Squared 1.00 No. of Observations 3.00 Degrees of Freedom 1.00  X Coefficient(s) 1.02 Std Err of Coef. 0.00  Deviation @ 2000 F(1093.3 K) = 1.29%
P2	273.30 371.80 447.60	273.60 373.60 450.80	Regression Output:  Constant -4.27 Std Err of Y Est 0.11 R Squared 1.00 No. of Observations 3.00 Degrees of Freedom 1.00  X Coefficient(s) 1.02 Std Err of Coef. 0.00  % Deviation @ 2000 F(1093.3 K) = 1.25%
P3	273.30 371.90 447.60	274.10 374.10 450.80	Regression Output:  Constant -2.96 Std Err of Y Est 0.03 R Squared 1.00 No. of Observations 3.00 Degrees of Freedom 1.00  X Coefficient(s) 1.01 Std Err of Coef. 0.00  % Deviation @ 2000 F(1093.3 K) = 1.11%
P4	273.30 371.80 447.60	273.60 373.60 450.80	Regression Output:  Constant -4.27  Std Err of Y Est 0.11  R Squared 1.00  No. of Observations 3.00  Degrees of Freedom 1.00  X Coefficient(s) 1.02  Std Err of Coef. 0.00  % Deviation @ 2000 F(1093.3 K) = 1.27%

Date <u>/9/0</u>			nermocouple numb	29.232/
		Reference: m	mercury-in-glass	_
Reference point number	Source <sup>b</sup> (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference,
0	ICE Bath	0	0	_
<b>_</b>	ROOM	25.5	26.1	0.6
				-

b<sub>Type</sub> of calibration system used.

$$\frac{\text{C}\left[\frac{\text{(ref temp, °C + 273)} - \text{(test thermom temp, °C + 273)}}{\text{ref temp, °C + 273}}\right]}{\text{ref temp, °C + 273}} ] 100 \le 1.5\%$$

\* MUST BE WITHIN 1°C OF REF

Quality Assurance Handbook M2-2.10

aEvery 30°C (50°F) for each reference point.

IMPINGER

\_\_\_ Thermocouple number 29.232/ Ambient temperature 26°C Barometric pressure 29.175 in. Hg Calibrator Garrison/ Reference: mercury-in-glass NBS SCOTT other Reference Thermocouple Reference thermometer potentiometer Temperature\_ Sourceb difference, point number a temperature, temperature, °C (specify) ICE 0  $\mathcal{O}$ BATH ROOM 0.6 26.6 26.0 TEMP

$$\begin{bmatrix}
\frac{\text{(ref temp, °C + 273)} - \text{(test thermom temp, °C + 273)}}{\text{ref temp, °C + 273}}
\end{bmatrix}$$
100<1.5%

\* MUST BE WITHIN POC OF REF

Quality Assurance Handbook M2-2.10

<sup>&</sup>lt;sup>a</sup>Every 30°C (50°F) for each reference point.

b<sub>Type</sub> of calibration system used.

Date	19/0ct 88	Th	ermocouple numb	IMPINGER er D3
Ambient te	mperature _	26 °C Baron	netric pressure ?	9.232/ 9.175 in. Hg
Calibrator	GARRISON/ SCOTT		nercury-in-glassother	NBS
Reference point number	Source <sup>b</sup> (specify)	Reference thermometer temperature, °C	Thermocouple potentiometer temperature, °C	Temperature difference,
C	ICE BATH	0	0.6	0.6
_	ROOM TEMP	25.8	25.6	0.2
				-
	<u> </u>			

\* MUST BE WITHIN I'C OF REF

Quality Assurance Handbook M2-2.10

<sup>&</sup>lt;sup>a</sup>Every 30°C (50°F) for each reference point.

b<sub>Type</sub> of calibration system used.

 $<sup>\</sup>begin{bmatrix} (\text{ref temp, °C + 273}) - (\text{test thermom temp, °C + 273}) \\ & \text{ref temp, °C + 273} \end{bmatrix}$  100<1.5%.

## TYPE S PITOT TUBE INSPECTION DATA FORM

#6B Pitot tube assembly level? \_\_\_\_\_ yes \_\_\_\_ no Pitot tube openings damaged? \_\_\_\_\_ yes (explain below) \_\_\_\_ no  $\alpha_1 = 0$  ° (<10°),  $\alpha_2 = 0$  ° (<10°),  $\beta_1 = 0$  ° (<5°),  $\beta_2 = / \circ (<5^\circ)$  $\gamma = 0$ °,  $\theta = 0$ °, A = 1/16 (in.)  $z = A \sin \gamma = O.D$  (in.); <0.32 cm (<1/8 in.),  $w = A \sin \theta = \frac{O.O}{cm}$  (in.); <.08 cm (<1/32 in.)  $P_A = \frac{17/32(0.53)}{(in.)} em (in.) P_b = \frac{17/32(0.53)}{(in.)}$  $D_{+} = 0.375 \in (in.)$ Comments: CONSTRUCTED 19W 40 CFR 60 APP A METH 2, FIG 2.2. ASSIGNED BOSELINE COEFFICIENT = 0.84 Calibration required? yes u no

Quality Assurance Handbook M2-1.7

 $D_{t} = _375 = (n.)$ 

Comments: CONSTRUCTED 14 W 40 CFR 60, 19PA, METHZ
F16-2.2 ASSIGNED BASELINE CUEFFICIENT = 0.84

Calibration required? \_\_\_\_\_ yes \_\_\_\_\_\_\_ no

Quality Assurance Handbook M2-1.7

NUTFCH #2

Date	JAN 89		Thermocouple numb	er NLEI /OU
Ambient te	emperature _		ometric pressure	
Calibrator		Reference:	mercury-in-glass	ASTM: 63F
	SCOTT		other	
Reference		Reference thermometer	Thermocouple potentiometer	Temperature b
point number	Source <sup>a</sup> (specify)	temperature, °C	temperature, °C	difference, *
VLET				
_	HOT WHELL BATH	43.5	43	. 5
_	ROM TEMP	26	26	0
tlet				
)	IN ARK	43.5	<b>47</b>	<i>!</i>
_	BATH	15	42	
	ROOM	26	26.5	.5

Quality Assurance Handbook M5-2.5

\* MUST BE WITHIN 3°C OF REFERENCE

aType of calibration system used.
b [(ref temp, °C + 273) - (test thermom temp, °C + 273)] 100≤1.5%.
ref temp, °C + 273

APPENDIX J
EPA Method 9 Certification Documentation

# The Texas Air Control Board Certifies That

PAUL T. SCOTT

Has completed a course conducted by The Texas Air Control Board and has met the requirements for evaluating visible emissions.



March 17, 1989

September 15, 1989

Children & Stanke 3/17/3

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